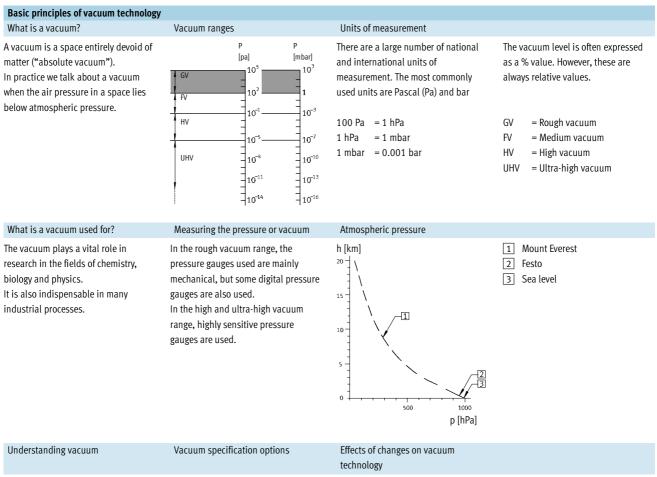
Introduction



Air is a gas mixture with approx. 10²⁵ particles per m³ of air at one bar air pressure. Particles exert pressure or force on the walls of a defined space. The fewer particles there are in the space, the

lower the force exerted on the walls.

$$Pressure = \frac{Force}{Area}$$

100% vacuum would mean that there are no particles present. Pressure = 0.

A vacuum can be specified as an absolute value, i.e. with a positive sign from 1 to 0 bar, with 0 as absolute zero. Or it can be specified as a relative value with a negative sign from 0 to -1 bar, with 0 as a reference point, or as a %.

As altitude increases, the air pressure in the atmosphere falls. This same effect reduces the attainable vacuum level of an ejector. Nevertheless, the performance level of 80% remains unchanged in this case.

Introduction

FESTO

Components for vacuum generation Vacuum ejectors

These function according to the venturi principle, i.e. they are driven purely pneumatically and have a much simpler design compared with other vacuum generators.

Displacement vacuum pumps Air flowing into a space is mechanically shut off, compressed and ejected. This allows a very high vacuum to be achieved at a very low flow rate.

Kinetic vacuum pumps

Air is forced to flow in the delivery direction through the application of additional mechanical force. This method achieves only a relatively low vacuum level despite a high suction rate.

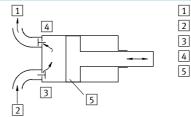
Principle

- The most important components are the jet nozzle (venturi nozzle) and at least one receiver nozzle.
- Accelerated compressed air generates a suction effect between both nozzles (vacuum).
- There are different design principles: single-stage and multistage ejectors.

• High vacuum level with relatively

Maintenance-free and wear-free

- Depending on the principle, air is either carried away in a flow by a rotating impeller on the suction side or compressed using vaned chambers.
- The pump types available include vacuum blowers and vacuum compressors, for example.



- Pressure side
 Suction side
 - 3 Inlet valve
 - Exhaust valve
 - Piston

- Low-weight, compact design
- Any mounting position
- High vacuum level up to -0.98 bar
- operating pressure
- Minimal maintenance expenses
- Generally large dimensions and high weight
- Restricted mounting position
- Large flow rates, low vacuum level
- High maintenance costs

Application

Low-cost

Features

small flow rate

- Wide range of applications, e.g. handling technology and process engineering.
- Broad application spectrum in industry and research.
- Used mainly for precision processes in industry.

Vacuum in handling technology				
Practical use of vacuum			Important selection factors	Benefits of a vacuum
The extensive range of vacuum component variants makes them ideal for use in many industrial applications.	Lifting Loading	Conveyance Turning Gripping Machining Holding Insertion Moving Repositioning orting	 Weight, temperature, shape and roughness of the workpiece surface Speed per unit of time Stroke travel and conveying distances 	 Gentle handling Compact, low-weight, space-saving design Fast cycle times possible Low maintenance costs Low-cost
Comparison of gigstors				

Comparison of ejectors		
Variables/criteria	Single-stage	Multi-stage
Suction flow rate	Average	High
		At low vacuum level up to approx. 50%
Evacuation time	Very short	Very short
	In higher vacuum range from 30 50%	In lower vacuum range up to 30 50%
Initial costs	Low	Relatively high
Noise generation	Relatively high	Low

Both principles have their advantages and disadvantages which are difficult to compare. With optimally adapted

components, both principles can cover a large number of different areas of application.

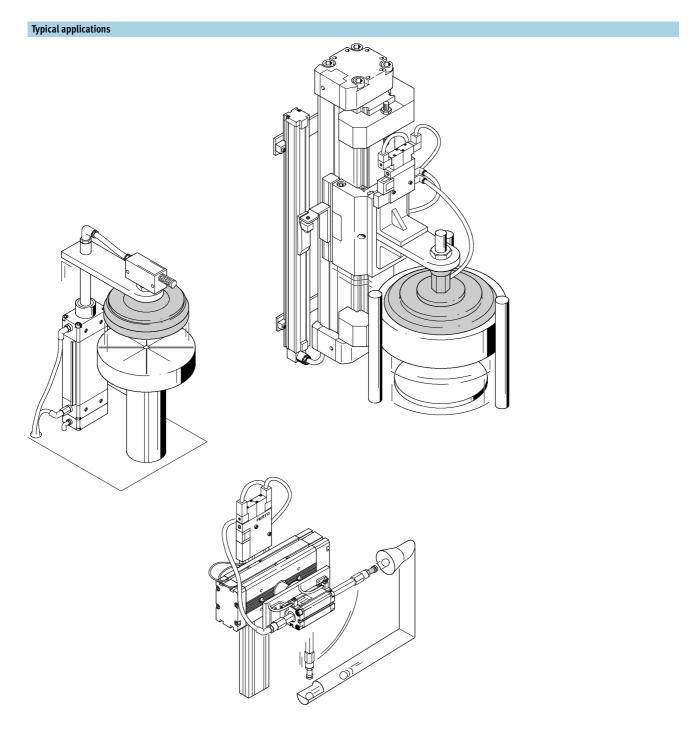
Important comparison variables			
Evacuation time	Air consumption	Efficiency	Suction flow rate
Evacuation time = Time (s) required to generate a specific vacuum.	Air consumption = Air consumption (l/min) of the ejector required to generate a specific vacuum.	The efficiency formula makes it easier to compare the different principles: Efficiency = Evacuation time, air consumption and volume dependent	The efficiency of an ejector is often – and incorrectly – measured using the suction flow rate at 0 bar.
		on vacuum.	Suction flow rate = Suction air volume

Suction flow rate = Suction air volume (l/min) that an ejector can draw in.

Vacuum in handling technology			
Energy cost comparison			
To generate compressed air from atmospheric air, you need to reckon on approx. € 0.02 per m ³ volume at 7 bar pressure when calculating the costs involved (e.g. investment, material, labour, etc.).	 Vacuum ejectors: High air consumption, but compensated by its energy-saving function Maintenance-free, no moving parts Low weight and component dimensions and can be installed in any mounting position No electrical connections required Relatively high vacuum level (up to 85% vacuum) attainable Low initial costs 	 Electric vacuum pumps: Very high vacuum (up to 99.99%) attainable High suction rates (vacuum blower) of up to 1,200 m³/hr. possible High current consumption because of continuously operated pumps High initial costs and ongoing maintenance costs Large weight and unit volume as well as fixed mounting position 	For a comparison of features, a calculation example and an energy cost comparison → following sections.
Leakage in vacuum systems			
When a vacuum suction gripper cannot fully seal the system against atmospheric air, we talk about leaking systems.	This might be caused, for example, by rough and uneven workpiece surfaces or air-permeable workpiece materials.	Remedial actions to achieve the required vacuum:Use of high-performance ejectorsReduction of the suction cup diameter	
Selection aid for vacuum generators			
In all cases, it is recommended that you perform a test setup to determine the leak rate, thereby enabling you to ascertain which vacuum ejector you need.	 Procedure: Determining the leak rate Perform the test setup Read the vacuum value achieved Compare the result with the course of the curve in the 'Suction capacity as a function of vacuum' chart (→ 28) Difference with respect to suction 	 Determining the correct ejector size Intersection of the leak rate (now known) with the curves of other ejectors Determine the attainable vacuum by means of projecting downwards from the intersections with the leak rate Select the ejector that reaches the 	

capacity = leak rate

required vacuum level.



Introduction

What is a vacuum?

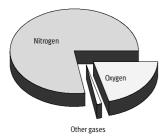
In physics, a vacuum is defined as "a state of emptiness that can be achieved by experiment" – in other words, nothing. This definition refers to the state of a space entirely devoid of matter (sometimes also referred to as an "absolute vacuum"). In practice, however, this state cannot be achieved. We therefore talk instead about a vacuum when the air pressure in a space is lower than the atmospheric pressure or when the density of air molecules is reduced. Furthermore, every space contains particles of matter such as protons and electrons, as well as zero-mass particles – photons – which transport energy at the speed of light.

What is a vacuum used for?

Since the 17th century ("Magdeburg hemispheres") mankind has been studying vacuum. Today, we cannot imagine modern research without it. In chemistry, reactions in substances are investigated in a vacuum, biology is interested in the effects of a vacuum on organisms, while some areas of physics (quantum physics, field theory, etc.) are concerned with particles that can be examined more accurately in a vacuum. Today, the vacuum plays a vital role in important industrial processes, many of which would not be possible without it. Noteworthy examples include semiconductor manufacture or mass spectroscopy. Vacuum technology has also played a part in the development and implementation of new ideas in handling technology, i.e. lifting, holding, rotating and transporting all kinds of parts.

Understanding vacuum

Air is a gas mixture containing approx. 10²⁵ particles per m³ at one bar air pressure.



In the atmosphere, this gas mixture is made up of the following gases and proportions:

- 78% Nitrogen
- 21% Oxygen
- 1% Other gases
 - (e.g. carbon dioxide and argon)

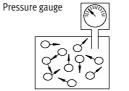
To attain a state of vacuum, a space must be empty, i.e. devoid of all gaseous material.

The consequence of this is that the pressure in this space is very low, as it contains no or only a small number of particles, which exert a force on an area as a result of their impact against the walls.

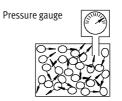
Pressure is therefore defined as follows:

Force Pressure =

In theory, in an absolute vacuum, i.e. where there are no more particles of matter in the space, pressure = 0.



Small number of particles at constant temperature → low pressure



Large number of particles at constant temperature

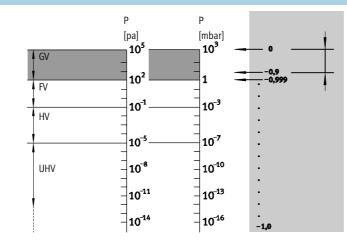
➔ high pressure

In reality, however, this is rarely achievable. In an ultra-high vacuum, the pressure may indeed be low (approx. 10^{-8} to 10^{-11} mbar), but the particle number density is still approx. 2.5×10^{13} particles per m³. The following rule therefore applies: **The fewer particles there are, the lower the pressure.**

Introduction

Vacuum ranges

In practice, the large vacuum range that can technically be achieved – which now consists of more than 16 powers of ten – is generally subdivided into smaller ranges. The vacuum ranges below are classified according to physical attributes and technical requirements.



Handling range: This vacuum range is used in handling

technology.

FESTO

- GV = Rough vacuum
- FV = Medium vacuum
- HV = High vacuum
- UHV = Ultra-high vacuum

Vacuum range	Pressure range (absolute)	Applications
Rough vacuum	Atmospheric pressure 1 mbar	Applications in industrial handling technology.
		In practice, the vacuum level is often specified as a percentage, i.e. the vacuum
		is defined in proportion to its ambient pressure. The material and the surface
		finish of workpieces play a major role in vacuum applications.
Medium vacuum	10 ⁻³ 1 mbar	Steel degassing, light bulb production, drying of plastics, freeze drying of
		foodstuffs, etc.
High vacuum	10 ⁻³ 10 ⁻⁸ mbar	Smelting or annealing of metals, electron tube manufacture.
Ultra-high vacuum	10 ⁻⁸ 10 ⁻¹¹ mbar	Spraying of metals, vacuum metallizing (coating of metals) as well as electron
		beam melting.

Measuring the pressure or vacuum

Pressure is defined as the force per unit area. Air is a gas mixture made up of many particles (atoms and molecules). These particles are in continuous motion. Wherever they meet, they exert a force. The pressure and vacuum are measured by taking a specific unit area and measuring the number and intensity of this impact on this area. Measurements are necessary in order to be able to check and monitor processes.



For this reason, all measuring instruments must be "calibrated", i.e. individual measuring instruments with the same function must be adjusted so that they produce the same result under the same conditions.

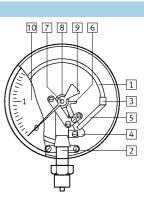
In order to be able to evaluate or measure the vacuum medium, there are a number of items of technical equipment that are indispensable for applications in the fields of industry and research.

Pressure gauges (vacuum gauges) are used generally as well as in the rough vacuum range. These gauges are scaled according to the level of accuracy required. Pressure gauges work according to many different operating principles and can function mechanically or digitally. The most common mechanical function types are:

- Bourdon tube pressure gauge
- Aneroid pressure gauge
- Diaphragm pressure gauge
- Digital pressure gauge

In the high and ultra-high vacuum range, pressure gauges with highly sensitive response mechanisms are used. A great many additional factors play a role in determining the measurement results in this case.

It is important to remember that there are two different options for specifying or representing the same measurement result.



Bourdon tube
 Spring support
 Spring end piece

- 4 Segment
- 5 Tie rod
- 6 Gearing
- 7 Indicator shaft
- 8 Coil spring
- 9 Indicator
- 10 Dial face

Introduction

Vacuum designations and specification options

It is important to mention at this point that there a number of different designations for the term vacuum in both colloquial and technical language. In order to avoid any uncertainty or

Vacuum as an absolute value

misunderstanding, these designations need to be explained here.

Vacuum

Correct designation – specified as % only in the range 0 ... 1 bar absolute pressure.

Operating pressure

Correct designation, operating pressure of 0 bar relative pressure is equivalent to 1 bar absolute pressure. A vacuum is generally specified as relative operating pressure, i.e. with a negative sign.

Operating pressure can be specified correctly in two different ways, i.e. as a relative or an absolute value. Both specification options are also applied to vacuums and are explained in more detail below.

Applications:	Ар
In the field of science as well as in the	In t
medium-high and high vacuum	ran
ranges.	Pri
Principle:	Vac
Vacuum is specified as an absolute	val
value in proportion to absolute zero,	pre
i.e. 0 bar is the lowest value and	val
corresponds to 100% vacuum. In the	the
vacuum range, 1 bar is thus the	pre
highest value and corresponds to the	refe
average ambient pressure.	low
Feature:	cor
Vacuum values have positive signs.	ope
Vacuum range 1 0 bar	Fea

Vacuum as a relative value plications: the rough or operating vacuum nge (e.g. for Festo applications). inciple: acuum is specified as a relative alue in proportion to ambient ressure, i.e. the specified vacuum lue has a negative sign, because e ambient pressure (atmospheric ressure) has been assumed as the ference point with a value of 0. The west value, i.e. also 100% vacuum orresponds to -1 bar relative perating pressure. ature: Vacuum values have negative signs. Vacuum range 0...-1 bar

Specification options for the pressure or vacuum				
Operating pressure	Vacuum	Absolute pressure		
[bar]	[%]	[bar]		
6	-	7		
5		6		
4		5		
3		4		
2		3		
1		2		
0	0	1		
-0.1	10	0.9		
-0.2	20	0.8		
-0.3	30	0.7		
-0.4	40	0.6		
-0.5	50	0.5		
-0.6	60	0.4		
-0.7	70	0.3		
-0.8	80	0.2		
-0.85	85	0.15		
-0.9	90	0.1		
-0.95	95	0.05		
-1	100	0		

Introduction

Units of measurement

As already described in the section "Designations and specification options", there are two ways of representing a vacuum:

- As a pressure unit
- (relative or absolute)
- As a percentage

There are a large number of national and international units of measurement in common use that can be used to specify a vacuum as a pressure unit.

These units of measurement are listed in the conversion table (international vacuum/pressure conversion table) below. It should be mentioned here that the current official unit of measurement for the vacuum is the pascal (Pa). However, this is rarely used in practice. In reality, the preferred units of measurement are bar, mbar or %, particularly in the rough vacuum range (e.g. handling technology). In the following pages also, only the units of measurement bar and % are used. Vacuum specifications that use bar as the unit of measurement are always considered as relative values (described under "Vacuum as a relative value").

The most commonly used pressure units bear the following ratios to one another:

100 Pa = 1 hPa 1 hPa = 1 mbar 1 mbar = 0.001 bar For the sake of simplicity, vacuum is generally expressed as a percentage in the range 0 to 100%. This is always a relative value. The conversion tables (international vacuum/pressure conversion tables) below are a useful aid for expressing these values relative to the other units of measurement.

Unit	bar	N/cm ²	kPa	atm, kp/cm ²	m H ₂ O	torr, mm Hg	in Hg	psi
bar	1	10	100	1.0197	1.0197	750.06	29.54	14.5
N/cm ²	0.1	1	10	0.1019	0.1019	75.006	2.954	1.45
kPa	0.01	0.1	1	0.0102	0.0102	7.5006	0.2954	0.145
atm, kp/cm ²	0.9807	9.807	98.07	1	1	735.56	28.97	14.22
m H ₂ O	0.9807	9.807	98.07	1	1	735.56	28.97	14.22
torr, mm Hg	0.00133	0.01333	0.1333	0.00136	0.00136	1	0.0394	0.0193
in Hg	0.0338	0.3385	3.885	0.03446	0.03446	25.35	1	0.49
psi	0.0689	0.6896	6.896	0.0703	0.0703	51.68	2.035	1

International vacuum/pressure conversion table with absolute and relative value comparison

, p								
Relative vacuum	Residual pressure, absolute	relative	N/cm ²	kPa	atm, kp/cm ²	m H ₂ O	torr, mm Hg	in Hg
[%]	[bar]	[bar]						
10	0.9	-0.101	-1.01	-10.1	-0.103	-0.103	-76	-3
20	0.8	-0.203	-2.03	-20.3	-0.207	-0.207	-152	-6
30	0.7	-0.304	-3.04	-30.4	-0.31	-0.31	-228	-9
40	0.6	-0.405	-4.05	-40.5	-0.413	-0.413	-304	-12
50	0.5	-0.507	-5.07	-50.7	-0.517	-0.517	-380	-15
60	0.4	-0.608	-6.08	-60.8	-0.62	-0.62	-456	-18
70	0.3	-0.709	-7.09	-70.9	-0.723	-0.723	-532	-21
80	0.2	-0.811	-8.11	-81.1	-0.827	-0.827	-608	-24
90	0.1	-0.912	-9.12	-91.2	-0.93	-0.93	-684	-27

Introduction

Atmospheric air pressure Definition

Our planet - which includes us as well as everything on the earth's surface - is surrounded by a layer of air several kilometres thick. This layer of air is known as the earth's atmosphere or, more simply, the atmosphere. Gravity causes the weight of this mass of air to exert pressure on the earth's surface. The pressure generated is known as atmospheric pressure or air pressure. Our atmospheric conditions can also be compared with conditions under water. We live at the bottom of a "sea of air"

The gravitational force of the air above us generates pressure which we call air pressure.

At present, the official unit of measurement for air pressure is hPa. This abbreviation stands for hectopascal (1 hPa = 1 mbar).

Generally applicable statements

- At sea level, atmospheric pressure is approx. 1,013 mbar.
- By 2,000 m above sea level, the pressure has fallen by approx. 1% per 100 m to 763 mbar.
- At approx. 5,500 m, the pressure is only 50% of the value at sea level.

On average, the air pressure at sea level is 1,013.25 mbar. If we imagine an air column with a cross-section area of 1 m², which extends from the earth's surface (sea level) to the outermost edge of the atmosphere, the air exerts pressure on this 1 m² of the earth's surface with a mass of 10,000 kg approx.

Note

NASA describes an altitude of approx. 120 km above the earth's surface as the outermost edge of the atmosphere. Air molecules can, however, be found at much greater altitudes. It is therefore impossible to definitively identify the "edge" of the atmosphere.

If, starting at sea level, we now begin to climb higher, this imaginary air column becomes shorter and the air mass is reduced. Because the air pressure falls as the air mass decreases, we can conclude that atmospheric air pressure falls as altitude increases. This is why we say that "the air is getting thinner".

Air pressure dependent on altitude can be calculated using the Boltzmann barometric equation. This calculation is affected by a wide variety of factors.

In order to achieve accurate results, it is important to consider not only the output altitude, but also factors such as local gravitational force, atmospheric density and temperature.

500

, 1000 p [hPa]

h [km]

20 -

15

10

0

To make things simpler, the air temperature and mass are considered as constants when deriving the formula.

In the derivation of the formula, the density of the layer of air (ρ) as well as the pressure at the earth's surface $(p_{(h=0)})$ are based on assumptions from empirical values. These courses of action and simplification of the formula derivation are an idealisation.

$$p(h) = p_{(h=0)} exp \left\{ \frac{-\rho \times gh}{p_{(h=0)}} \right\}$$

- p(h) = Air pressure dependent on altitude
- = Pressure at the earth's $p_{(h=0)}$ surface (1.013 bar)
 - = Density of the layer of air (1.29 kg/m^3)
 - = Altitude
 - = Acceleration due to gravity
- 1 Mount Everest
- 2 Festo

ρ

h

g

3 Sea level

- At the summit of Mount Everest (8,848 m), atmospheric pressure is only 330 mbar. • At an altitude of 16,000 m the
- pressure is 90 mbar, while it is 15 mbar at 30,000 m and approx. 8 mbar at 50,000 m.



Introduction

Effect of changes in air pressure on vacuum technology

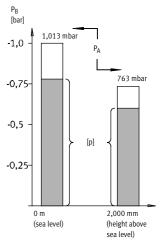
The pressure drop that occurs with increasing altitude does, of course, have an effect on vacuum technology or even on the vacuum generators themselves.

Because the air pressure in the atmosphere falls with increasing altitude, the maximum attainable differential pressure and, consequently, the maximum attainable holding force of a vacuum suction gripper are also reduced. In other words, the attainable vacuum level of a vacuum ejector reduces with increasing altitude. Nevertheless, the performance level of 80% vacuum, for example, remains unchanged (→ Figure on right). As described earlier, air pressure at sea level (0 m) is approx. 1,013 mbar. At sea level, a vacuum generator with a performance level of 80% vacuum achieves absolute pressure of approx. 0.2 bar (200 mbar). This air pressure falls with increasing altitude. Up to a height of 2,000 m, there is a linear drop in pressure by approx. 12.5 mbar per 100 m to 763 mbar.

However, although the same vacuum generator still has the same performance level of 80% vacuum, this figure of 80% refers to the ambient pressure that has fallen to 763 mbar because of the increase in altitude. This vacuum generator can therefore only achieve a maximum absolute pressure of approx. 0.4026 bar (402.6 mbar).

Assuming that we take the same vacuum generator and go higher than the previous 2,000 m above sea level in order to generate or use a vacuum, the maximum attainable vacuum level would continue to fall while the performance level would remain unchanged at 80% because the ambient pressure in the atmosphere continues to drop.

At a height of approx. 5,500 m above sea level, the air pressure is only approx. 50% of the pressure value at sea level (506 mbar). The possible holding force of a vacuum suction gripper falls proportionally with the attainable vacuum value.



p = Performance of vacuum generator X = 80%

Valid standards and guidelines

In accordance with Festo standard FN 942 011, the standards and guidelines have been defined for the vacuum range.

Vacuum:

All vacuum generators based on this standard that are covered in this system description operate exclusively in the rough vacuum range. In accordance with the Festo guideline, the average air pressure at sea level (1,013.25 mbar) must always be taken as the reference value when specifying and calculating pressure values.

Scaling factor:

When measuring characteristics (air consumption, pressure, evacuation time and suction capacity), fluctuations in the ambient pressure must be taken into account. Given that all pressure values measured in the research laboratory are relative pressure values referring to the current ambient pressure, the fluctuations in ambient pressure result in a degree of dispersion in the measurement results.

The measurement results are therefore related to the reference pressure. They are converted using a scaling factor (S), which is calculated on the basis of the following equation.

$$S = \frac{p_{ref}}{p_{amb}}$$

(p_{ref} = 1,013 mbar)

Example:

A current air pressure $p_{amb} = 975$ mbar produces a scaling factor S = 1.039. The required vacuum is therefore produced at a measured value of 750 bar (0.75 mbar) absolute to P = 780 bar (0.78 mbar).

DIN standards, research reports and Festo guidelines

DIN 1 314 Pressure, basic definitions and units

DIN 28 400 Vacuum technology Part 1 General terms Part 2 Vacuum pumps Part 3 Vacuum gauges Part 8 Vacuum systems, components DIN 28 402 Quantities, symbols and units (summary)

Graphical symbols (summary)

DIN 28 401

FB 190 Vacuum Guideline – Basic Principles (Research Report, Festo Research, Dr. Berger) FR 970 003 Fluid Units and Variables

FR 970 004 Flow Rate Measurement

Introduction

Vacuum generator Introduction

Generating a vacuum in a closed space means dropping the air or gas pressure. To do this, the gas particles must either be removed or reduced in quantity.

There are basically two ways of doing this:

 The gas is evacuated from the closed space into an external space or into the atmosphere.
 The gas is combined within the vacuum system, i.e. condensed, absorbed or chemically combined. The range of vacuum generators is very extensive. All work according to different technical principles and methods and are often categorised under the umbrella term "vacuum pumps".

We need to categorise the vacuum generators into three types here and classify them according to their mode of operation:

- Vacuum ejectors,
- Gas-absorbing vacuum pumps,
- Gas-feeding vacuum pumps.

A direct comparison of these vacuum generators would not be objective enough, as they differ fundamentally from one another in terms of their technical construction, their mode of operation, their ranges of application and their efficiency. In this section we will describe the various types of vacuum generator referred to here based on their

functionality and focus on their

technical features and benefits.

Vacuum ejector - High vacuum, relatively low flow rate

General

Compared with the often highly complex and unwieldy mechanical designs used to generate a vacuum, the operating principle of ejectors is extremely simple. Yet despite its simplicity, this principle offers enormous potential as an extremely practical solution. Vacuum ejectors basically function according to the venturi nozzle principle, i.e. the vacuum is generated using pneumatically driven nozzles without moving parts. Vacuum ejectors are characterised by their ability to generate a high vacuum or low pressure with a relatively low flow rate.

They operate according to two different design principles using very different, often complex equipment such as valves, filters, silencers, switches, etc. However, the crucial element that they have in common is the fact that the venturi principle is applied wherever the vacuum is generated.

Function principle

A classic ejector consists of a jet nozzle (venturi nozzle) and, depending on the design principle, at least one receiver nozzle. Compressed air enters the ejector. The narrowing of the jet nozzle (venturi nozzle) accelerates the air to up to 5 times the speed of sound as it flows through the jet nozzle. There is a short gap between the exit from the jet nozzle and the entry in the receiver nozzle. The expanded compressed air from the jet nozzle creates a suction effect at the gap to the receiver nozzle, which in turn creates a vacuum at the output (vacuum port). Single-stage ejector

Venturi nozzle (jet nozzle) Receiver nozzle



12

Vacuum ejector – High vacuum, relativ	vely low flow rate		
Design principles			
Single-stage ejector: The design principle for a single-stage ejector includes a jet nozzle and only one receiver nozzle. After exiting the receiver nozzle, the exhaust air is generally discharged via a silencer or directly into the atmosphere.	Multi-stage ejector: This design principle also includes a jet nozzle. Behind the first receiver nozzle there are additional nozzle stages, each of which has a bigger nozzle diameter in proportion to the	falling air pressure. The drawn-in air from the first chamber, combined with the compressed air from the jet nozzle, is thus used as a propulsion jet for the other chambers.	Again, the air is generally discharged via a silencer at the end of the last receiver nozzle.
Features			
 Completely maintenance-free and wear-resistant because there are no moving parts Low initial costs Low energy costs, as the ejector is only switched on when in use 	 No heat build-up Compact design, smallest possible dimensions Suitable for pulsed applications Fast reacting 	 Small line lengths between vacuum generation and application Easy to install, can assume any mounting position Low weight 	 Multiple functions possible in a single device Dry and filtered compressed air is useful Supply port 4 6 bar optimal
Applications			
 Part feeding systems in the automotive industry Packaging inductor 	 Industrial robot applications in all sectors 	Process engineering	 Transport of liquids and bulk material

• Packaging industry

Subject to change

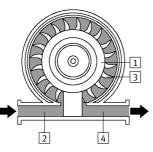
Displacement/kinetic vacuum pumps			
General			
Another component for generating a vacuum is the vacuum pump.	In order to come up with a useful classification of the pump designs and operating principles used in vacuum technology, it is best to subdivide them according to their method of operation.	Vacuum pumps Gas-absorbing Gas-fee Vacuum pumps Vacuur Displacement Vacuum pumps	rding n pumps Kinetic Vacuum pumps
Gas-absorbing vacuum pumps			
Function principle			
As their name suggests, gas-absorbing vacuum pumps do not discharge the gas particles, but instead convert	them into a liquid, solid or sorptive state within the vacuum system. In this way, the volume of gas (air) in the	closed space is reduced and a vacuum is created.	
Gas-feeding displacement vacuum pur	nps – High vacuum, low flow rate		
Function principle			
In displacement vacuum pumps, the gas (air) freely enters an expanding space, and is then mechanically shut off, compressed and ejected. The main feature of vacuum pumps of this type is the fact that they can achieve a very high vacuum with very low flow rates.	The figure on the right is a simplified illustration of how the principle of a displacement vacuum pump works. Although there is a wide range of solutions with varying designs, the operating principle of all pumps is the same.		 Pressure side Suction side Inlet valve Exhaust valve Piston
Features			
 High vacuum level of up to 98% attainable 	• Minimal maintenance expenses	 Generally restricted mounting positions 	Larger dimensions
Applications			
 Packing machines 	Manual vacuum handling	Clamping devices	• Research

Introduction

FESTO

Gas-feeding kinetic vacuum pumps – Low vacuum, high flow rate Function principle With kinetic vacuum pumps, the gas particles (air) are forced to flow in the delivery direction through the Vacuum blowers are categorised as kinetic vacuum pumps. These vacuum generators operate application of additional force during evacuation. according to the impulse principle, i.e. during the transfer of kinetic

The main feature of these vacuum pumps is that only a relatively low vacuum can be generated. However, they do achieve very high flow rates (high suction capacity) at the same time. Vacuum blowers are categorised as kinetic vacuum pumps. These vacuum generators operate according to the impulse principle, i.e. during the transfer of kinetic energy to the air by a rotating impeller 1, the air is drawn in and compressed 4 on the suction side 2 by the blades 3 on the impeller.



Vacuum compressors are another type of kinetic vacuum pump with similar features.

The drawn-in air is compressed in the vaned chambers of an impeller in multiple stages with low pulsation by means of centrifugal force. As with the blower, high suction rates can be achieved here with limited vacuum performance.

Features			
Vacuum blowers and compressors	• Large volumes extracted in a very short time	High maintenance costs	Only low vacuum performance possible
Applications			
Vacuum blowers	 Handling of extremely porous materials such as clamping plates or cardboard boxes, etc. 	• Where large suction rates per unit of time are important	
Compressors	• For precision industrial applications		

Introduction

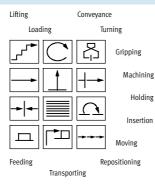
Practical use of vacuum

Handling is a subfunction of material flow and is subdivided into the areas of storing, changing quantities, moving, securing and checking. Handling requires the availability of specific geometric bodies (component parts or assemblies). Among the equipment used in handling technology are feed technology components and systems, pick-andplace devices, manipulators and robots.

The way in which parts are handled has a major influence on productivity in automated production and assembly processes today. Vacuum technology is now an important part of this handling technology and has become indispensable in many of the industries and fields of application in which it is used. Vacuum technology has proven to be extremely effective in the handling of a wide variety of materials and parts and has thus opened up entirely new areas of application and solutions for handling technology.

Handling tasks

The following keywords and symbols illustrate the significance of vacuum technology in handling technology as well as the various tasks that it is used to perform.



All of these tasks combined cover an almost unlimited range of applications in industry.

Industrial fields of application of vacuum technology include, for example:

- Special machine construction
- Packaging industry
- · Food industry
- Woodworking industry
- Metalworking industry
- Automotive industry
- Electrical engineering industry

General

Vacuum technology generally tends to come under the umbrella term of gripper technology.

In handling technology, a large number of applications use mechanical gripper technology to great effect.



Nevertheless, there are also a great many applications where this technology is being pushed to its limits.

This is where vacuum technology frequently comes into play and, indeed, is creating entirely new concepts and possibilities.



Advantages

Vacuum in handling technology means:

• Gentle handling of fragile parts

Important factors to consider

The decision to use vacuum technology or another handling technology depends on a number of different factors. Some of the most important factors to consider are described here.

- Simple component and system design
- Compact, space-saving design

• Weight of the workpiece

surface

completion

• Temperature of the workpiece or its

• Speed per unit of time for cycle

• Shape of the workpiece surface

• Stroke travel and conveying

distances for handling

• Roughness of the workpiece surface

- Low weight, i.e. suitable for extremely dynamic movement
- Fast cycle times possible

Having such a wide range of vacuum component variants makes it easy to find the right components for just about any application, taking into account the above factors, with product features such as heat resistance, speed, suction capacity etc.

- Low-cost
 - Low maintenance costs
 - Can be adapted to suit many requirements

Festo provides a software tool which helps you select or find the right vacuum components for your specific applications.

Introduction

Single-stage and multi-stage ejectors			
General			
Nowadays, wherever vacuum technology is used, you will also find increased use of vacuum ejectors.	There are, of course, still a great many special applications in which the vacuum pump is as indispensable as ever. Nevertheless, many applications in handling technology favour the use	arguments in favour of ejectors are their low initial costs, low maintenance costs and greater flexibility in terms of application compared with other vacuum	As already explained in the section "Components for vacuum generation → 2, there are two different design principles for vacuum ejectors. How ever, the venturi operating principle

Function principle

As described earlier, all ejectors work according to the venturi operating principle.

All ejectors based on this principle have a jet nozzle (laval nozzle) and,

of ejectors. The most convincing

compared with other vacuum generators.

depending on the design principle, at least one receiver nozzle.

n ion' gn owever, the venturi operating principle applies to both types.

FESTO

Design principle

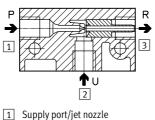
Single-stage ejector:

This ejector principle includes a jet nozzle (laval nozzle) and one receiver nozzle.

The extraction of ambient air and the generation of a vacuum therefore take place within a chamber and the gap between the jet nozzle and receiver nozzle.

The compressed air or drawn-in ambient air is generally discharged into the atmosphere (environment) via a silencer connected directly after the receiver nozzle.

Single-stage ejector:



Vacuum/suction cup connection 2 3 Exhaust air/receiver nozzle

Multi-stage ejector

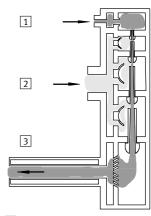
Like the single-stage ejector, this design principle also includes a jet nozzle (laval nozzle), in which the compressed air flowing in is accelerated to up to five times the speed of sound, followed by a receiver nozzle.

Behind the first receiver nozzle there are additional nozzle stages, each of which has a bigger nozzle diameter in proportion to the falling air pressure. The drawn-in air from the first chamber, combined with the

compressed air from the jet nozzle, is thus used as a propulsion jet for the other chambers.

After exiting the last receiver nozzle, the exhaust air is generally discharged into the atmosphere (environment) via a silencer.

Multi-stage ejector



1 Supply port/jet nozzle

- 2 Vacuum/suction cup connection
- 3 Exhaust air/receiver nozzle

Subject to change

Introduction

Single-stage and multi-stage ejectors Basic information

A direct comparison of the design principles of single-stage and multistage ejectors frequently gives rise to discussions regarding the advantages and disadvantages of both principles. Manufacturers of vacuum ejectors tend to favour one of the two design principles, thus making it difficult to get an objective opinion. Viewed objectively, handling technology using a vacuum comes down to a few important variables, with which the performance of a vacuum generator can be measured or evaluated.

Efficiency η as a function of vacuum Δp_u

Evacuation time = Time (s) required to generate a specific vacuum.

Air consumption = Air consumption (l/min) of the ejector required to generate a specific vacuum.

These variables – evacuation time, air consumption and the volume dependent on the vacuum – produce a formula, which can be used to calculate the efficiency of a vacuum generator. This is the most objective criterion that can be used to assess the performance of different vacuum generator types.

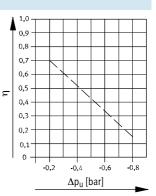
$$\eta(\Delta pu) = \frac{1}{1 + \frac{t(\Delta pu) \times Q}{V \times 60 s/min}}$$

- η(Δpu) = Efficiency of the vacuum
 generator in relation to
 low pressure
- $t(\Delta pu) = Evacuation time [s]$

Q

V

 Air consumption [l/min]
 Volume to be evacuated (standard volume) [l]



In practice, the job of a vacuum generator is to generate a specific vacuum in the shortest time possible, using as little air (energy) as possible.

Misapprehension

Suction flow rate = Suction air volume (l/min) that an ejector can draw in. In practice, the performance of an ejector is often – and incorrectly – measured on the basis of the suction flow rate. The misapprehension lies in the fact that the suction flow rate is often measured at atmospheric pressure and the result is then used as the ejector rating. In fact, the suction flow rate falls progressively with an increasing vacuum, i.e. a high suction flow rate does not necessarily result in a short evacuation time. Performance comparisons of vacuum ejectors based on the suction flow rate therefore have only a limited level of accuracy. Apart from this, the suction flow rates of the specimens are compared at the same vacuum level.

Introduction

Single-stage and multi-stage ejectors

Comparison

a 10 11

The aim of this comparison of singlestage and multi-stage ejectors is to evaluate variables or criteria that occur in practice and that can be used to measure the performance of the ejectors.

- Evacuation timeAir consumption
- Efficiency

Variables such as noise level, air supply time or attainable vacuum also play an important role. A comparison of single-stage and multi-stage ejectors in practice produces the following general observations, which should be borne in mind before proceeding any further.

General findings		
Variables/criteria	Single-stage	Multi-stage
Suction flow rate	Average	High
		At low vacuum level up to approx. 50%
Evacuation time	Very short ¹⁾	Very short ¹⁾
	In the higher vacuum range from 30 50%	In lower vacuum range up to 30 50%
Initial costs	Low	Relatively high
Noise generation	Relatively high	Low

1) see diagram below

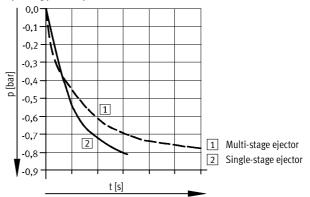
Evacuation time

In general, the multi-stage ejector can, up to a pressure range of approx. 30 ... 50% vacuum, generate this pressure faster or evacuate the volume faster than the single-stage ejector. However, a pressure of

 $-0.4 \dots -0.8$ bar or a vacuum of between 40 and 80% is normally required in practice.

Looking at the chart illustrating this comparison, it is obvious that singlestage ejectors have a clear advantage over multi-stage ejectors in this case. The higher the vacuum level, the more time the multi-stage ejector takes to generate it.

Operating pressure p as a function of the evacuation time t



Air consumption

Multi-stage ejectors have, on average, a much lower level of air consumption and thus consume less energy than single-stage ejectors, giving them a clear advantage over single-stage eiectors.

However, if we look at this information in context with the evacuation time,

the advantage is not so clear-cut. Although multi-stage ejectors have a lower level of air consumption, their evacuation time is higher. This considerably reduces the energysaving benefits.

Suction flow rate

Single-stage ejectors have a lower suction flow rate than ejectors based on the multi-stage principle. Multistage ejectors in the low vacuum range of approx. 30 ... 50% can thus draw in higher volumes over the same amount of time. However, as the vacuum level increases (from approx. 30 ... 50%), this progressive curve falls off rapidly for multi-stage ejectors (see chart). In other words, as pressure increases, the initial gains of a higher suction rate fall below the values achieved with single-stage ejectors.

Introduction

Single-stage and multi-stage ejectors

Noise level, vacuum level and air supply time

In comparison, single-stage ejectors have a relatively high level of noise generation. Because the compressed air is slowed down by the series of nozzle stages before it reaches the

the case of multi-stage ejectors, the noise level is, accordingly, lower than with single-stage ejectors. The noise levels in single-stage ejectors are,

atmosphere in "weakened" form in

however, counteracted with suitable silencers.

Both design principles reach the same vacuum level, although single-stage ejectors do so in a shorter time.

another, are changed.

Although increasing the laval nozzle diameter while maintaining a constant operating pressure increases the suction rate, it also extends the evacuation time and, in extreme cases, the desired vacuum cannot be reached without increasing the

There are very few differences in air supply time, although a single-stage ejector has a smaller volume to supply with air, which gives them a minimal time advantage.

Summary

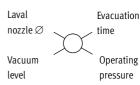
The cause of the somewhat poorer evacuation time of the multi-stage ejector lies in the fact that although the second and subsequent nozzle stages generate a high suction capacity, these are decoupled at a relatively low vacuum level. This means that when the pressure is higher, only the first nozzle stage draws in air. This first nozzle stage is

considerably less efficient than a single-stage ejector. It is important, however, to remember that these findings must be viewed as generalisations and should therefore be used for reference purposes only. Irrespective of the design principle, different results are obtained when the initial values, which interact with one

operating pressure.

This example illustrates how all of these variables are dependent on each other. If one variable changes,

this affects the other variables as well.



Conclusion

The comparison shows just how difficult it is to reach an objective conclusion about the pros and cons of both operating principles. And that's to say nothing of deciding on a preferred operating principle or a "test winner". Basically, the benefits of both principles lie in very specific areas and they justify their right to

exist on this basis.

It is also easy to see how minor technical adjustments affect the ejectors and how both operating principles can be optimised to suit the relevant application (e.g. by varying the laval or receiver nozzle diameter). Both operating principles can thus achieve degrees of efficiency or

possess attributes that defy any generalisation. In conclusion, it can be said that the single-stage ejector achieves its best results in applications with average or higher pressure (vacuum). The simple design makes this operating principle more costeffective and, in terms of dimensions, more manageable than the multistage principle.

The multi-stage ejector, on the other hand, achieves its best results wherever a relatively low vacuum (up to approx. -0.3 bar) needs to be generated quickly and wherever energy costs play an important role.

Introduction

Energy cost comparison between vacuum ejectors and vacuum pumps (electric)

Given that energy is a scarce, valuable and, above all, expensive resource, energy costs play an important role in choosing a suitable vacuum system. The air consumption of a vacuum system might not initially seem to be a particularly important consideration. However, the amount of energy that is necessary to operate a pneumatic vacuum ejector with compressed air cannot be overlooked. You should therefore remember one golden rule at all times: air is expensive.

With electrically driven vacuum pumps, on the other hand, energy costs can be measured and assessed much more easily on the basis of current consumption. The fact is that in order to generate compressed air from atmospheric air, taking into account all costs such as material, depreciation, labour costs, etc., with electricity tariffs (industry) of € 0.10/kWh, you must reckon on costs of approx. € 0.02 per 1 m³ volume at 7 bar (normal supply pressure). These costs apply in the low pressure range up to 10 bar. In the high pressure range (10 ... 20 bar), the costs for compressed air increase by approx. 100%.

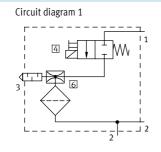
FESTO

Before proceeding any further, it is important that we mention some of the criteria that should be considered when making a comparison of vacuum ejectors and vacuum pumps.

Vacuum ejector

For

- Energy consumed only as required. Compressed air or energy is only consumed during the suction operation and during "workpiece handling" in an operation cycle. The vacuum generator remains switched off for the rest of the time (discharge, return). Ejectors have fast response times (start and stop times) and can therefore be switched off when no vacuum is required (→ circuit diagram 1).
- Vacuum ejectors require absolutely no servicing apart from the prefilter and have no moving parts.



- 1 = Compressed air connection
- 2 = Suction cup connection
- 3 = Exhaust port
- 4 2/2-way valve
- 6 Non-return valve
- Energy-saving function: Many ejectors (compact ejectors) have this function. Compressed air is only consumed during generation of the vacuum. Once the vacuum level has been reached, the ejector is switched off. The vacuum is maintained and monitored using valves and switches

(→ circuit diagram 2).

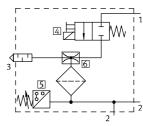
Energy-saving function =

4 2/2-way valve +

5 Switch +

- 6 Non-return valve
- Their low weight/mass ratio and their small unit volume, not to mention the fact that they can be installed in any mounting position, are also worth noting.
- A relatively high vacuum of up to 85% can be attained.





1 = Compressed air connection

- 2 = Suction cup connection
- 3 = Exhaust port
- 4 2/2-way valve
- 5 Switch
- 6 Non-return valve

Against

- With Festo ejectors, the suction rate is relatively limited at approx. 16 m³/hour.
- Higher compressed air consumption per m³ vacuum increases energy costs dramatically. However, this is compensated by the air/energysaving functions.

Introduction

Vacuum pump For • With some designs a very high • High suction rates of up vacuum level (up to 10⁻⁴ mbar to 1,200 m³/hr. possible. = 99.99999%) can be attained. Against • Electro-mechanical vacuum pumps • High initial costs and ongoing • Large weight/mass ratio and large are almost always in continuous maintenance costs. unit volume as well as fixed operation, the vacuum requiremounting positions. ments are regulated by means of valves. This means that current consumption and, consequently, energy costs are very high. Energy cost comparison/sample calculation In this example, we are comparing a • The electricity price is based on • The costs for compressed air refer • Additional assumed numerical vacuum ejector (pneumatic), both industry tariffs (€ 0.10/kWh). to, as mentioned earlier, a 1 m³ values such as time specifications, with and without an air-saving volume with 7 bar pressure. All for example, may apply depending on the application. function, with a vacuum pump costs such as material, depreci-(electrical) of similar performance. ation, labour costs, etc. are taken Using a calculation example, we want into account in the calculation to create a cost or energy cost (€ 0.02/m³). comparison over a period of one year.

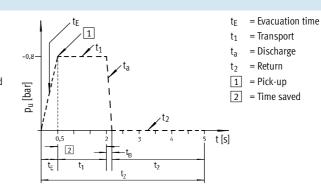
Electricity price	Compressed air costs	System capacity	Remarks
[€/kWh]	[€]	[kW]	
0.05	0.02	approx. 1,100	Large system
0.10	0.02	approx. 1,100	Large system
0.10	0.03	approx. 20	Small system

Introduction

Calculation base Ejector operation cycle

- Ejector with air-saving function: Air consumed (energy consumption) only while the workpiece is being received (picked up) (= 0.5 s).
- Ejector without air-saving function: Air consumed (energy consumption) for reception (pick-up) and transport of the workpiece (= 2 s).
- Vacuum pump: Energy consumed for the entire operation cycle, as the pump is not normally switched off (= 5 s).

The figure on the right shows an operation cycle for a vacuum system. The individual work steps of the system are subdivided into time sectors. The amount of time allocated to the work steps depends on the vacuum generator.



Variables/criteria		Assumed numerical values
Initial costs for vacuum pump	[€]	715
Initial costs for ejector	[€]	337
Maintenance costs/year for vacuum pump	[€]	306
No. of operating days/year		250
No. of operating hours/day		16
Time per operation cycle	[s]	5.0
Time for pump ON	[s]	5.0
Time for ejector ON ¹⁾	[s]	2.0
Time for ejector ON ²⁾	[s]	0.5
Price per kWh (industry tariff)	[€]	0.10
Price per m ³ for compressed air at 7 bar	[€]	0.02
Supply pressure for ejector	[bar]	6
Energy used to generate compressed air $(1m^3 \text{ at } p = 7 \text{ bar})$	[kWh/m ³]	0.095

1) Without air-saving function

2) With air-saving function

General calculations

When comparing the energy costs for both vacuum generators, the following calculations must first be performed:

- Number of products per year (hours)
 Formula: Total running time (s)/Time per operation cycle (s)
 = 250 x 16 x 3,600/5 s
 = 2,880,000 hours
- Proportion of pump operation to operation cycle (%)
 Formula: Time for pump ON (s)/ Time per operation cycle (s) x 100
 = 5/5 x 100

= 100%

 Proportion of ejector operation without air-saving function to operation cycle (%)
 Formula: Time for ejector ON¹⁾ (s)/Time per operation cycle (s) x 100
 = 2/5 x 100

= 40%

 Proportion of ejector operation with air-saving function to operation cycle (%)
 Formula: Time for ejector ON²⁾(s)/Time per operation cycle (s) x 100
 = 0.5/5 x 100
 = 4%



Introduction

Vacuum ejector calculation

The calculations for the vacuum ejector with and without the airsaving function give us the following partial results:

 Running time per year Formula: No. of products (units) x Time for ejector per unit (s) 2,880,000 unit x 2 s
 1) = 5,760,000 s (96,000 min)
 2) = 1,440,000 s (24,000 min) (air consumption at P = 6 bar: 505 l/min)

 Air consumption per year Formula: Running time per year (min)/ Air consumption (l/min) 96,000 min/505 l/min
 1) = 48,480 m³
 2) = 12,120 m³ • Energy costs per year Formula: Air consumption (m^3) x Price per m^3 for compressed air (\in) 48,480 (12,120) $m^3 x \in 0.02$ $1^1 = \notin 969.60$ $2^1 = \notin 242.40$

Variables/criteria		Assumed numerical values
Air consumption at P = 6 bar	[l/min]	505
Total air consumption per year at P = 6 bar ¹⁾	[m ³]	48,480
Total air consumption per year at P = 6 bar ²⁾	[m ³]	12,120
Air saving per year ²⁾	[m ³]	36,360
Air saving per year ²⁾	[%]	75
Energy costs per year ¹⁾	[€]	969.60
Energy costs per year ²⁾	[€]	242.40
Energy saving per year ²⁾	[€]	727.20

1) Without air-saving function

With air-saving function

Electric vacuum pumps calculation

The calculations for the vacuum pump give us the following partial results:

- Running time per year
 Formula:
 Operating hours per day
 x Operating days per year
 16 hours x 250
 = 4,000 hours
- Energy consumption per year Formula: Running time per year x Energy consumption per hour 4,000 hours x 0.55 kW
 = 2,200 kWh
- Energy costs per year Formula: Energy consumption per year x Costs per kWh
 2,200 kWh x € 0.10
 = € 220

Variables/criteria		Assumed numerical values
Energy consumption/operating hour	[kWh]	0.55
Energy consumption/year	[kWh]	2,200
Energy costs/year	[€]	220

Introduction

Introduction			
Cost comparison of the vacuum eject	or and vacuum pump		
The costs of the vacuum system are made up of three cost types:	 Investment costs Maintenance costs Energy costs 	Investment costs are one-off costs, while maintenance and energy costs are incurred annually.	

Result

A direct cost comparison shows that the vacuum pump has the lowest energy costs, closely followed by the ejector with the air-saving function.

The ejector without the air-saving function has considerably higher energy costs than the other vacuum systems. If we also take maintenance

and investment costs into account, this reduces the advantage that the vacuum pump has over the other systems due to its low energy costs.

Cost type	Vacuum pump	Ejector without air-saving function	Ejector with air-saving function
Investment [€]	715	337	337
Maintenance ¹⁾ [€]	306	-	-
Energy ¹⁾ [€]	220	969.60	242.40

1) annual costs for a vacuum pump after approx. 4,000 to 6,000 hours

Conclusion

The calculation example shows that ejectors more than justify their existence. The high investment costs for vacuum

pumps as well as the annual

maintenance costs associated with their continuous use and wearing parts confirm this conclusion. While ejectors may use more energy, their simple design keeps initial costs and maintenance costs to a minimum. There are, of course, a great many areas of application that are

dominated by the vacuum pump and where ejectors are not used. This is not the case, however, with handling technology.

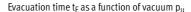
Introduction

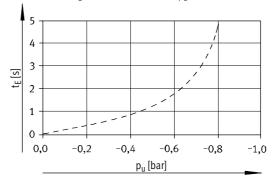
Leakage in vacuum systems

Ideally, when using vacuum applications in handling technology, the workpiece surfaces on which the suction cups have to rest should be smooth and impervious. A suction cup fits tightly against this type of surface. When a vacuum is generated, the sealing rim of the suction cup can fully seal the system against external atmospheric air. We therefore describe this as a leak-proof system. The holding force of the suction gripper on the workpiece increases as the vacuum level in the system increases compared with the external atmospheric pressure. Unfortunately, these ideal surface conditions do not always exist on the workpieces to be moved. The materials are often air-permeable (e.g. sheets of paper) or very rough and uneven. In these applications, the vacuum suction grippers cannot completely seal the system against atmospheric air. If atmospheric air constantly enters the system during vacuum generation, we describe this as a leaking system.

Leak-proof systems

In vacuum technology, the performance of the vacuum generator for the handling of leak-proof material depends, among other things, on how quickly the system can generate a specific vacuum. This rating is known as the evacuation time of the vacuum generator. When a specific volume is being evacuated, the course of the time/ pressure curve travels upward proportionally, i.e. the higher the vacuum level, the stronger the fall in the suction capacity of a vacuum generator and the longer it takes to attain an even higher vacuum level.



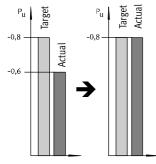


Leaking systems

The requirements for handling porous materials (leaking systems) are different. In order to attain or maintain the desired vacuum level, the vacuum generator must be capable of

Remedy

In general, there are two options for optimising or increasing the vacuum level in leaking systems.



continuously evacuating the air (leakage air) entering the system. The maximum attainable vacuum that a vacuum generator can produce is normally measured under ideal

Using a high-performance vacuum

· Power transmitted as required

Option 1:

generator.

Advantage:

• Simple solution

• Leakage remains high

· High energy costs

Disadvantage:

conditions (leak-proof system). However, in this case the leakage air entering the system prevents the vacuum generator from reaching or being able to attain its maximum performance level. To determine the leakage air volume, it is recommended that you carry out a test (\rightarrow 27, "Selecting vacuum generators according to leakage flow").

Option 2:

Reducing the suction cup diameter or orifices.

Advantage:

- Leakage is reduced (energy costs) Disadvantage:
- Power transmission may be below the required vacuum level.

To select the correct vacuum generators for handling leakage flow, you need to perform a test setup as outlined above. With the aid of charts, you can then select the right vacuum generator.

This selection aid is described in detail on page 27.

Introduction

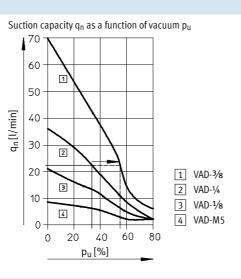
Selecting vacuum generators according to leakage flow

A reliable method is needed to determine the exact leak rate in vacuum systems or applications. Only then can optimal remedial action,

Graphical representation as a tool

Graphical representation
 of the suction capacity in relation to
 vacuum/operating pressure in a
 chart (all ejectors in a single chart).

e.g. the selection of vacuum generators with larger dimensions, be taken and the functional reliability of the vacuum system guaranteed.

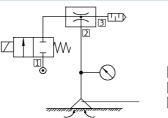


All curves in the chart have an almost linear downward course. The maximum suction capacity of the individual vacuum ejectors is reached at atmospheric air pressure (0% vacuum).

The higher the vacuum level, the lower the suction capacity of a vacuum generator, up to a maximum limit. This chart is very useful for finding out quickly and reliably whether a vacuum generator is needed to achieve the desired vacuum level with leaking materials.

Test setup

Perform a test setup
with an ejector as the vacuum
generator, a vacuum gauge
(pressure gauge) as the measuring
instrument as well as a suction
gripper and workpiece as the
leakage source. The test setup is
illustrated in the following figure.



Supply port
 Suction cup connection
 Exhaust port

The operating pressure (vacuum) of the system is now measured at a constant supply pressure. The performance of an ejector under normal operating conditions, i.e. without leakage, can be determined from its technical data as well as from the 'Suction capacity as a function of vacuum/operating pressure' chart. The measurement results from the test setup are then compared with the known data.

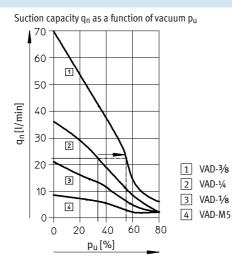
Selecting vacuum generators according	g to leakage flow		
Procedure			
Where systems are clearly leaking (e.g. because of porous or rough workpieces), the leak rate must be determined.	The following procedure is recommended for finding a suitable vacuum generator that is compatible	with the relevant application and can generate the required vacuum level:	
Determining the leak rate			
 Perform the test setup Read the vacuum or operating pressure achieved Compare the result with the course of the curve in the chart Suction capacity difference = leak rate 	In a test setup like the one illustrated earlier, a workpiece is picked up using a defined suction gripper size, a vacuum generator and pressure supply (5.5 6 bar).	In a leak-proof system, the value indicated on the vacuum gauge must correspond to the value contained in the technical data for the vacuum generator. In a leaking system, the vacuum attained is read from the vacuum gauge.	The leak rate can then be determined on the basis of the measured vacuum value in conjunction with the chart (Suction capacity as a function of vacuum/operating pressure).
Example			
n a test setup using the ejector 2 VAD-1/4, a vacuum level of 35% is achieved at full pressure supply. Starting from this result, if we draw a horizontal line and a vertical line intersecting the ejector curve 2, the	residual airflow can be read from the suction capacity scale. This residual airflow corresponds to the leak rate of the system, as in the case of a leak-proof system the residual airflow would be = 0.	Result: The residual airflow or leak rate is = 22 l/min. The only disadvantage of this method lies in the fact that it is impossible to tell whether the leakage is caused by the workpiece itself or by a rough surface underneath the edge of the suction gripper.	
Determining the correct ejector size			
 Compare the intersection of the leak rate (now known) with the curves of other ejectors. Determine the attainable vacuum by projecting the intersections with the leak rate downwards. Select the ejector that reaches the required vacuum level. 	Conversely, with a known leak rate of 22 l/min, we can now read the vacuum level attainable with other vacuum generators from the "Suction capacity as a function of vacuum" chart.	If we now extend the horizontal line that we drew previously in the chart to determine the leak rate (Procedure 1), we can determine the vacuum level attained with other vacuum	generators (at the same leak rate) from the intersection with the curves of other ejectors and the subsequent downwards projection to the vacuum scale.

Introduction

Selecting vacuum generators according to leakage flow

Example

If we extend this horizontal line, it must intersect another curve. In the case of the next largest vacuum generator 1 VAD-3/8, the line intersects at 52% vacuum. The curve for the next smallest vacuum generator 3 is overshot and there is no intersection. In other words, the low performance value would mean that no vacuum is generated with this leakage flow, as the quantity of air drawn in is lower than the quantity of air that is discharged because of the leakage.



Result:

In this application, the next largest vacuum generator 1 would attain a vacuum level of 52%. If this vacuum level were sufficiently high for the application, this would be the right choice of ejector. Otherwise, a higher-performance ejector should be chosen (curves not available in this chart).

FESTO

Conclusion

This method is useful for determining the correct ejector size where the leak rate is known.

- e.g.:
- seals,tubing connectors,

However, it should be noted that

leakage can occur at other positions,

- couplings
- in a vacuum system.

Leakage, for whatever reason, should be avoided if at all possible.

• Safety risk A leakage flow increases the risk of the vacuum system no longer being able to attain the required pressure

and the workpiece being dropped

during handling.

• Energy costs Where there is a leakage flow, the air consumption (energy consumption) of an ejector is much higher than that of a leak-proof system.

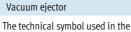
• Time

A leakage flow means it takes longer to reach the required vacuum level.

Introduction

Technical symbols

This system description uses technical symbols to represent individual components in function charts as well as in component descriptions. These symbols are illustrated and described in this section.



function charts for all Festo vacuum generators.



Vacuum gauge

Measuring and checking device for the analogue vacuum display.

Filter

Filters the drawn-in air and prevents

contamination of the ejector.

Reservoir container

previously picked up.

Air reservoir to support the setting

down of a workpiece that was

For controlling the flow rate or



Vacuum suction cups

Standard, extra-deep, round, oval. In technical circuit diagrams, this symbol represents the complete suction gripper (suction cup holder + suction cup + accessories).



Bellows suction gripper

1.5 convolutions, 3.5 convolutions. In technical circuit diagrams, this symbol represents the complete suction gripper.

back against the intake direction, i.e. the valve permits flow in one direction only.

Prevents the drawn-in air from flowing



Non-return valve

Solenoid valve

Different valve types (mostly 2-way valves) perform the ON/OFF or exhaust function in vacuum technology.





Throttle

pressure.

Silencers

Dampens the compressed air, which flows from the venturi nozzle at ultrasonic speed, before it is discharged into the atmosphere.

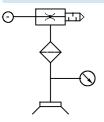


Introduction

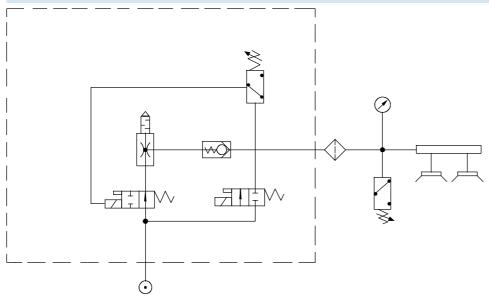
Circuit diagrams with vacuum components

Circuit diagrams help provide a general understanding of the mode of operation of vacuum components as well as a schematic representation of their function within the overall system. The technical drawings below contain examples of pneumatic circuit diagrams. These are intended as a reference to help you understand the symbols used in vacuum technology.

Basic vacuum circuit



Regulated vacuum circuit



Introduction

Vacuum ejectors

Vacuum generators are the central element of any vacuum system. The mode of operation of vacuum ejectors and the venturi principle were already explained in the Basic principles section (\rightarrow 12).

Festo only uses ejectors that operate according to the single-stage design principle.

Festo offers a wide selection of ejectors of different types and with different equipment to suit a whole host of application and performance requirements.

These vacuum generators are subdivided into the following ejector groups:

- Basic ejectors
- Inline ejectors
- Compact ejectors

Each group is, in turn, subdivided into a wide range of performance classes and equipment types.

Because they are so compact, ejectors

of this type can generally be used

required, even in large quantities.

processes that do not require complex

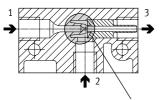
and sophisticated control technology.

directly wherever a vacuum is

They are also used in vacuum

Standard and inline ejectors

The functions of standard and inline ejectors are essentially limited to the basic function of an ejector, i.e. generation of a vacuum.



Ejector/venturi nozzle

VN-

- 1 = Compressed air / nozzle
- 2 = Vacuum / suction port
- 3 = Exhaust air/receiver nozzle

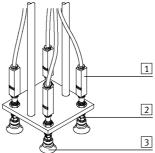
The ejector design basically consists of just a single jet nozzle that operates according to the venturi principle.



VAD-...

Control, monitoring and other functions depend on external and additional components within the vacuum system.

These ejectors are therefore much smaller compared with other vacuum ejectors.



9

Ejector
 Suction cup holder

3 Suction cup

Introduction

Compact ejectors

In practice, demands on vacuum systems in terms of function, speed (performance) and, increasingly, economy tend to be extensive. Vacuum ejectors are therefore capable of much more than just vacuum generation. Compact ejectors have a number of components integrated in or on the housing, which makes them complete function units. Depending on the ejector and design, these function units contain the following components in addition to the vacuum generator:

- Solenoid valves
- Filter
- Non-return valves

FESTO

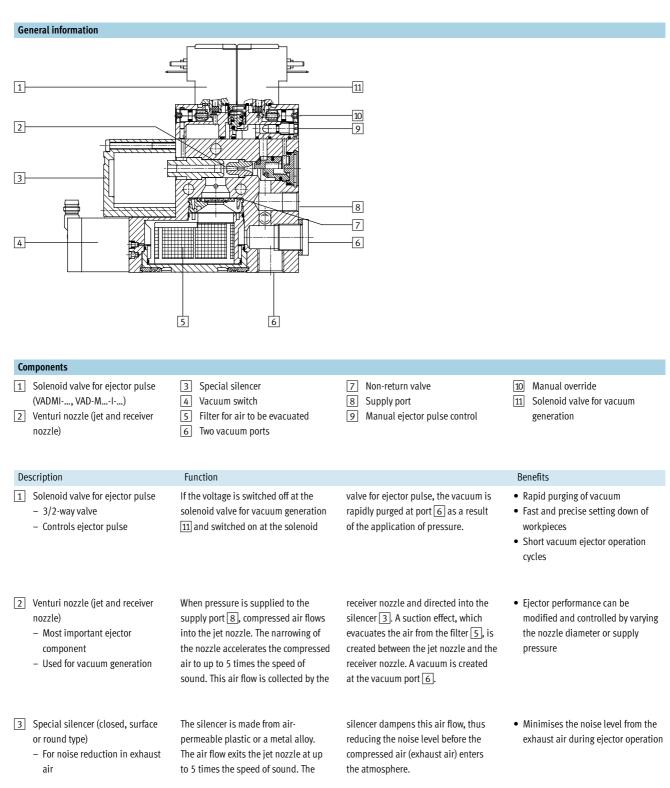
- Silencers
- Vacuum switch

Vacuum ejector VADMI-...



Taking a vacuum ejector VADMI--... as an example, we can see the components and functions of a complete function unit. The individual components are identified in the sectional drawing $(\rightarrow 34)$. The functions, benefits and special features are described in the notes.

Introduction

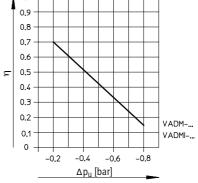


		_	
	_		_

Components			
Description	Function		Benefits
 4 Vacuum switch with PNP or NPN output For pressure monitoring 	On the vacuum switch, the vacuum range for holding the workpiece is set using two potentiometers. Once the vacuum level is reached, a signal switches off the vacuum generator (air-saving function). The non-return valve 7 maintains the vacuum in this	status. If the vacuum range falls below the required level, the signal controls the switching on of the vacuum generator. If the required vacuum can no longer be generated because of a malfunction, the vacuum generator is switched off.	 Air-saving function: The vacuum generator is switched off within the required vacuum range Safety function: Control of vacuum generator if vacuum level goes above or below the required values
 Filter for air to be evacuated With contamination indication 40 μm grade of filtration 	A large plastic filter is integrated between the vacuum port 6 and the vacuum generator 2 or non-return valve 7. During the suction	operation, the air is filtered before it enters the vacuum generator. A removable display window shows the degree of filter contamination.	 No contamination of the system Protection of components Display ensures maintenance is carried out regularly
 Two vacuum ports (V) or (2) With female thread 	Vacuum components can be connected here (e.g. vacuum suction gripper).	Depending on the application, you can use either one output or both outputs simultaneously.	
Built-in non-return valve	After the vacuum generator is switched off, this non-return valve prevents a backflow of the drawn-in	air, thus preventing a drop in pressure.	• The vacuum is maintained after the vacuum generator is switched off (air-saving function in connection with the vacuum switch 4).
8 Supply port (P) or (1)	The compressed air supply port (P) or (1) for generating the vacuum is con- tained in the ejector housing.		
9 Manual ejector pulse control	The intensity of the air flow and, consequently, the time taken to remove the workpiece from the	suction gripper, can be adjusted manually.	• The system can be optimised for the vacuum application
10 Manual override	Stem on the solenoid valve that can be switched without an electrical signal. However, an electrical signal	that is already present cannot be disabled.	 Manual switching of the solenoid valve
 Solenoid valve for vacuum generation 3/2-way valve Controls vacuum generation 	When the signal is activated, compressed air flows through the vacuum generator and creates a	vacuum. The air flow is interrupted when the signal is turned off.	• Air-saving function in connection with the vacuum switch 4 and the non-return valve 7

Important variables		
Selecting a suction gripper		
The main criteria to consider when selecting a suction gripper:	• Total volume of the vacuum system	Cycle time of an operation Ejector economy Additional functions
Total volume		
The sum of the volumes is needed to calculate the cycle time of an operation.	The volume to be exhausted from the system is made up of the following:	Suction cup volumeSuction cup holder volumeTube volume
Cycle time of an operation		
When defining quantities, the time factor plays a decisive role. The evacuation time is used to determine how economical an ejector is.	 Individual criteria for determining the duration of an operation cycle: Evacuation time: Time taken for the ejector to generate the required vacuum Air supply time: Time taken to set down the workpiece under suction (purging of the vacuum) Handling/return time 	Evacuation time t _E for 1 l volume at 6 bar operating pressure p_u $30 \xrightarrow{27}{24}$ $10 \xrightarrow{27}{24}$ 10
Ejector economy		
Factors for determining the energy consumption of an ejector:	 Air consumption per unit of time (specified in the ejector technical data) Number of operation cycles per unit of time 	Air consumption q_n as a function of operating pressure p_1
Comparison of vacuum generators		
Efficiency is a criterion which facilitates an objective comparison of various vacuum generator types.	The product section of this catalogue contains information to help you determine the efficiency of an ejector (→ 18)	Efficiency η as a function of vacuum Δp_u at P_{nom} 6 bar 0.9 0.8

(**→** 18). The chart allows you to compare the efficiency curves of other vacuum generators.



Suction grippers			
General data Vacuum suction grippers provide the "link" between the vacuum generator and the workpiece being transported.	They are a simple, low-cost and reliable solution for handling workpieces, parts, packaging, etc.	Festo offers a wide range of suction gripper designs:	 Universal suction gripper Flat suction gripper Bellows suction gripper Special suction gripper
Mode of operation			
When the suction gripper comes into contact with the workpiece surface, the same air pressure (atmospheric pressure) prevails on the top side and underside of the suction cup. The activated vacuum generator now	draws in the air on the underside of the suction cup. A vacuum is created. Given that air pressure within the vacuum is lower than that on the outside of the suction cup,	atmospheric pressure holds the workpiece on the suction cup. The larger the vacuum, the greater the holding force pressing the suction cup onto the workpiece.	
Materials			
The suction cups are available in different materials. • Nitrile rubber • Polyurethane • Polyurethane, heat-resistant • Silicone • Fluoro rubber • Butadiene rubber, anti-static	 Depending on the range of application, the following conditions play an important role when deciding on the quality of the materials to be used: Resistance to wear Intensity of stress Industry in which gripper is to be used (food industry, electronics) Workpiece quality (surface, weight, sensitivity, etc.) Environment (chemically aggressive media, temperatures) 	The criteria for selecting the right suction cup material are summarised in a table (→ 44).	
Shapes			
Suction grippers can move a wide variety of workpieces. The range of workpiece surface structures and contours available demands versatile gripper technology. Vacuum technology allows a wide	variety of products and materials (shapeless, compact or porous) with a wide variety of surfaces (even, uneven, round, sloping or undulating) to be handled easily, cost-effectively and, above all, reliably.	Furthermore, it is possible to pick up workpieces with masses ranging from a few grammes right up to several kilogrammes.	
Accessories			
For every suction cup there is a suction cup holder to fit. Depending on their design, these can be used for a variety of applications.	The suction cup holders are characterised based on the following criteria: • Holder size • Suction cup connection • With or without height compensator • Position and type of vacuum port	Suction cup holders are more than just mounting devices for suction cups.	

• Mounting thread

→ Internet: www.festo.com/catalogue/...





Introduction

Suction grippers

Advantages of a bellows suction cup

When the volume of a bellows suction cup is evacuated, the suction cup shape contracts slightly. The workpiece is lifted gently in the process. In practice, this so-called flexible vertical stroke can be used as a short vertical stroke to lift workpieces gently from their supports.

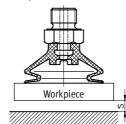
The evacuation of a bellows suction cup is divided into 2 phases:

Phase 1 The suction cup is positioned on top of the workpiece without the influence of any external forces.



Phase 2

A vacuum is created within the suction cup. The workpiece is drawn in and a state of equilibrium is achieved depending upon the size of the vacuum and the weight of the workpiece.



Suction gripper selection guidelines

When designing a suction gripper for a specific handling task, there are several criteria to be taken into consideration:

Parameter	Effects on							
		Required suction	No. of suction cups	Suction cup shape	Suction cup material			
		force						
Workpiece dimensions		•	•	-				
Workpiece weight		•	•	•				
Workpiece rigidity		-	•	•				
Surface texture of the workpiece	Harsh	•	•	•	•			
	Dry, wet	•	•	-				
	Round, diagonal, curved	-	-	•				
Environmental influences such as								
weather, cleaning agents, approval for		-	-	-				
use in the food industry, temperature								
Distribution of suction grippers on the				_				
workpiece		-	-					
Arrangement of suction gripper in								
relation to direction of movement		-	-	-				
Max. acceleration		•	-	-				

Introduction

Physical variables

The physical variables described below are components of the formulae that are needed to calculate the main criteria.

Coefficient of friction µ

The coefficient of friction is the friction factor between the suction gripper and workpiece. It defines the tangential forces.

In practice, it is very difficult to obtain precise specifications for this value. Suitable experiments should therefore be carried out for the relevant application.

In order to be able to select a design, the following theoretical guide values apply:

Surfaces	
Oily	μ = 0.1
Wet	μ = 0.2 0.3
Rough	μ = 0.6
Wood, metal,	
glass, stone	$\mu = 0.5$

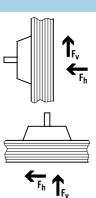
Safety value S

The regulations for the prevention of accidents (UVV) stipulate a safety factor of 1.5. This minimum value must be incorporated in the calculations.

In the case of critical, non-uniform or porous materials or rough surfaces, the factor should be increased to ≥ 2 . The safety value is also important for the position of the suction gripper.

A higher factor should also be selected in the case of a vertical suction gripper position or swivel motions.

With a horizontal suction gripper position, where the applied load acts vertically on the suction cup, a value of between 1.5 and 2 may be used.



Theoretical holding force T_H

This force is calculated with a dry surface for the various load conditions of the application. The following factors are taken into account in this formula:

- Mass of the workpiece m
- Coefficient of friction µ
- Acceleration of the system (m/s²) • Acceleration due to gravity (9.81 m/s²)
- Safety value S

Only the result from the most unfavourable application load condition is taken into consideration.

Breakaway force FA

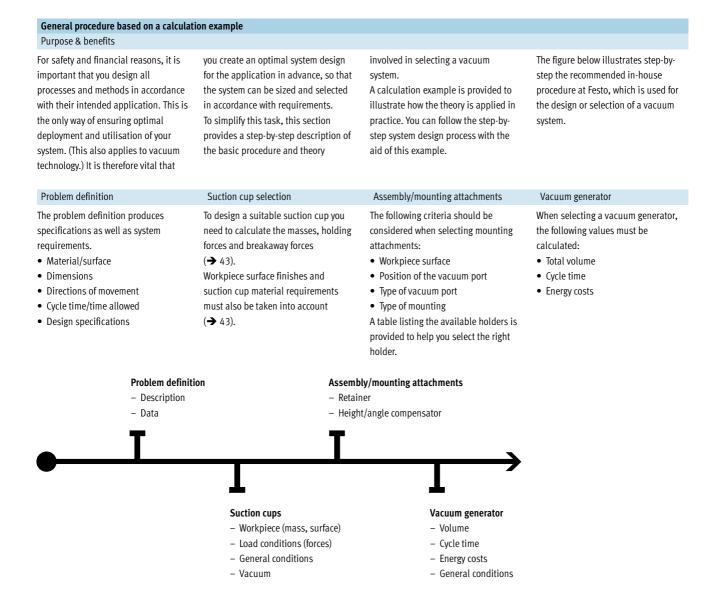
The breakaway force depends on the suction cup diameter and suction cup shape.

If several suction grippers are used simultaneously in a vacuum

application, the result of the theoretical holding force T_H calculation must be divided by the number of suction grippers.

This allows you to determine the holding force of each suction gripper. The breakaway force of the selected suction cup must always be greater than the determined holding force T_H. When selecting a suction gripper, you can refer to the suction cup technical data to find out its breakaway force.

Introduction



Introduction

Software tool

As a special service Festo offers you free software. The software tool in question is a reliable, convenient and,

above all, quick way of designing your vacuum systems. It allows you to specify the vacuum components of

Concession and part of			1.1
in releases	sjorm pjon sjor pj		
	Products		
			P0570
- 2 -			10.010
4			Name Table College
100			Cater Manualar
11	Here products	·O-	inter-
	Postario words	-#=	
	Image search		
	Dexid weeds	90	
9			
Contraction (see a)			

your system individually and select suggested products from the Festo range.

Software tool: Vacuum selection



Vacuum selection software www.festo.com/en/engineering

FESTO



周 And and the And

Selection program for calculating the mass of the workpiece

Program for selecting the suction gripper

Subject to change

Introduction

Problem definition

Problem

definition

Assembly/ mounting components Suction Vacuum generator cups transported from point 1 to point 2 Specifications for the workpiece and general conditions for the vacuum system are listed in the section below (assumed values) and should be

2

Vacuum system, comprising:

necessary calculations.

referred to when performing the

A workpiece of mass X is to be

using a vacuum system.

- Suction cups
- Assembly/mounting attachments
- Vacuum generator

We need to find out which vacuum system from the Festo product range is the right one for this application. To do this, we need certain values or forces (required values).

1

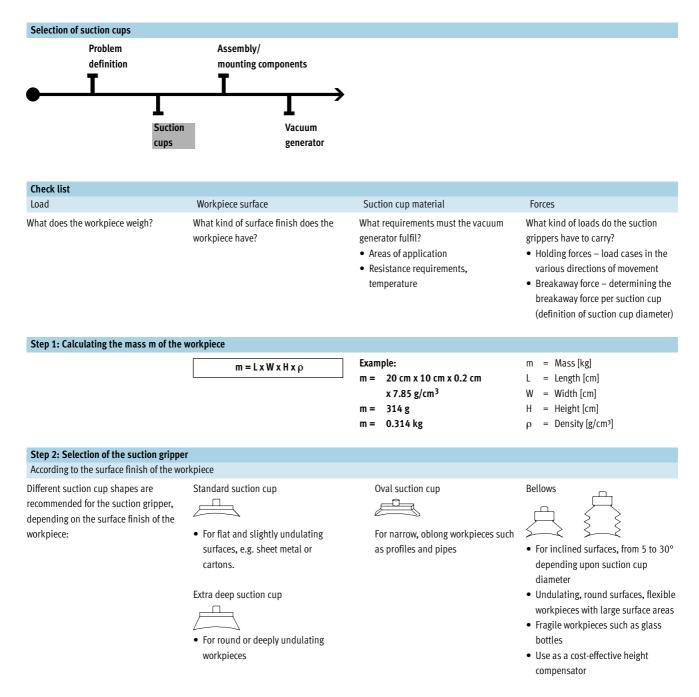
Assumed values				Required values
For the workpiece		For the handling system		
Material	Sheet steel	Compressed air supply	6 bar	The values specified below must be
Surface	Even, smooth, slightly oily	Directions of movement	Lift vertically	calculated to determine the correct
	(e.g. from the press)		Travel horizontally	vacuum system.
Dimensions	Length: 200 mm		90° Rotate	Other general conditions must be
	Width: 100 mm		Travel vertically	taken into account here.
	Height: 2 mm	Max. acceleration	5 m/s ²	The following sequence is
		Cycle time	max. 3.5 s	recommended:
		Time requirements	For picking up: < 0.5 s	 Mass (weight) of the workpiece
			For setting down: 0.1 s	 Holding force and force of
		Safety factor	1.5	acceleration
		Design		Total volume
		conditions	2 suction grippers for	Cycle time
			vibration-free transport;	
			spring-action picking up/	Other general conditions
			setting down of the workpiece;	 Material and surface finish
			vacuum line ports at side;	 Height and angle compensation

suction grippers mounted

using male threads.

Costs

Introduction



Result

If, in the sample exercise, we were using sheet steel with an even, smooth surface, a standard suction cup would be the best solution.

Step 2: Selection of the suction gripper

According to the material quality of the workpiece

Depending on the application, the following conditions need to be taken into consideration:

- Life expectancy
- Environment (e.g. chemically aggressive media, temperatures)
- There are different material designs available, such as:
- For smooth or rough surfaces
- For high temperatures
- Antistatic design for electronics components

• Continuous load in multiple shift operation

Material properties		Nitrile rubber	Polyurethane	Polyurethane (heat-resistant)	Silicone	Fluoro rubber	Butadiene (anti-static)
Material code		Ν	U	Т	S	F	NA
Colour		Black	Blue	Red-brown	White transparent	Grey	Black with v dot
Resistance to wear/ resistance to abrasion		**	***	***	*	**	**
Areas of application							
Very high stress		-	*	*	*	-	-
Food processing		-	-	-	*	-	-
Oily workpieces		*	*	***	-	*	*
High ambient temperatures		-	-	-	*	*	-
Low ambient temperatures		-	*	*	*	-	-
Smooth surface (glass)		*	*	*	-	*	-
Rough surface (wood, stone)		-	*	**	-	-	-
Antistatic		-	-	-	-	-	*
Minimal marking		-	*	*	*	-	-
Weather			**	**	***	***	
Resistance to tearing		**	***	***	*	**	**
Resistance to tearing Permanent deformation		**	***	***	* *	**	**
*					* ** -		
Permanent deformation	ic oil	**	*	**	* ** -	***	**
Permanent deformation Mineral based hydraulic oil		**	*	**	-	***	**
Permanent deformation Mineral based hydraulic oil Synthetic ester based hydrauli		** *** *	* *** -	** *** -	-	*** *** *	** - -
Permanent deformation Mineral based hydraulic oil Synthetic ester based hydrauli Non-polar solvents (e.g. white		** *** *	* * * - **	** *** -	-	*** *** *	** - - -
Permanent deformation Mineral based hydraulic oil Synthetic ester based hydrauli Non-polar solvents (e.g. white Polar solvents (e.g. acetone)		*** * *** * *** * *** * *** * *** ** **	***	** ** - **	- - - -	*** *** * * * * * *	** - - - -
Permanent deformation Mineral based hydraulic oil Synthetic ester based hydrauli Non-polar solvents (e.g. white Polar solvents (e.g. acetone) Ethanol Isopropanol Water		** *** * *** - ***	*** - ** - ** - ** - **	** *** - ** - - - - - -	- - - - *** ***	*** * * * * * * * * * * * * * * * * *	** - - - - - -
Permanent deformation Mineral based hydraulic oil Synthetic ester based hydrauli Non-polar solvents (e.g. white Polar solvents (e.g. acetone) Ethanol Isopropanol Water Acid (10%)		** ** * * * * * * * * * * * * * * * *	* *** - ** - ** - ** - - * - - - - - - - - - - -	** *** - ** - - - - - -	- - - - *** ***	*** * * * * * * * * * * ***	** - - - - - - - - - - - -
Permanent deformation Mineral based hydraulic oil Synthetic ester based hydrauli Non-polar solvents (e.g. white Polar solvents (e.g. acetone) Ethanol Isopropanol Water Acid (10%) Alkaline (10%)	spirit)	** *** - *** ** ** ** ** ** ** ** ** **	*** ***	** *** - ** -	- - - - *** *** ** ** ** **	*** *** *	** - - - - - - - - - - - - - - - - - -
Permanent deformation Mineral based hydraulic oil Synthetic ester based hydrauli Non-polar solvents (e.g. white Polar solvents (e.g. acetone) Ethanol Isopropanol Water Acid (10%) Alkaline (10%) Temperature range, long-term	spirit)	** *** * *** - *** *** *** - *** *** *** ** - ** ** ** ** **	* *** ** * * * * * -20 +60	** *** - ** - - - - - - - - - - - - -		*** *** * * * * * * * * * *	** - <
Permanent deformation Mineral based hydraulic oil Synthetic ester based hydrauli Non-polar solvents (e.g. white Polar solvents (e.g. acetone) Ethanol Isopropanol Water Acid (10%) Alkaline (10%)	spirit)	** *** - *** ** ** ** ** ** ** ** ** **	*** ***	** *** - ** -	- - - - *** *** ** ** ** **	*** *** *	**
Permanent deformation Mineral based hydraulic oil Synthetic ester based hydrauli Non-polar solvents (e.g. white Polar solvents (e.g. acetone) Ethanol Isopropanol Water Acid (10%) Alkaline (10%) Temperature range, long-term	spirit)	** *** * *** - *** *** *** - *** *** *** ** - ** ** ** ** **	* *** ** * * * * * -20 +60	** *** - ** - - - - - - - - - - - - -		*** *** * * * * * * * * * *	** - <
Permanent deformation Mineral based hydraulic oil Synthetic ester based hydrauli Non-polar solvents (e.g. white Polar solvents (e.g. acetone) Ethanol Isopropanol Water Acid (10%) Alkaline (10%) Temperature range, long-term Shore hardness A	spirit)	** *** * *** - *** ** - *** - ** **	* ***	** *** - ** - - - - - - - - - - - - -		*** *** * * * * * * * * * * * * * * *	** - - - - - - - - - - - - -
Permanent deformation Mineral based hydraulic oil Synthetic ester based hydrauli Non-polar solvents (e.g. white Polar solvents (e.g. acetone) Ethanol Isopropanol Water Acid (10%) Alkaline (10%) Temperature range, long-term Shore hardness A	spirit)	** *** * *** - *** ** - *** - ** **	* ***	** *** - ** - - - - - - - - - - - - -		*** *** ** *** - ** *** ** *** ** ** **	** - - - - - - - - - - - - -
Permanent deformation Mineral based hydraulic oil Synthetic ester based hydrauli Non-polar solvents (e.g. white Polar solvents (e.g. acetone) Ethanol Isopropanol Water Acid (10%) Alkaline (10%) Temperature range, long-term Shore hardness A	spirit)	** *** * *** - *** ** - *** - ** **	* ***	** *** - ** - - - - - - - - - - - - -		*** *** * *** * *** *** ***	** - - - - - - - - - - - - -

Result

For the workpiece in the problem example we would choose a suction cup made from polyurethane (material code U).

Introduction

case

case)

Step 3: Calculating the holding force and breakaway force Determining the holding force To determine the holding force you Note need to know the mass of the workpiece, on the one hand, and the The forces of acceleration that operate designing a suction gripper system. acceleration, on the other. in a fully automatic system must be taken into consideration when Case 1 Example: Horizontal suction gripper position, $F_{H} = m x (g + a) x S$ vertical direction of movement (best $F_{H} = 0.314 \text{ kg x} (9.81 \frac{\text{m}}{\text{s}^{2}} + 5 \frac{\text{m}}{\text{s}^{2}}) \times 1.5$ $F_{\rm H} \approx 7~{ m N}$ Case 2 Example: Horizontal suction gripper position, $F_{H} = m x (g + \frac{a}{\mu}) x S$ $F_{\rm H} = 0.314 \, \text{kg x} \, (9.81 \, \frac{\text{m}}{\text{s}^2} + \frac{5 \, \frac{\text{m}}{\text{s}^2}}{0.1}) \, \text{x} \, 1.5$ horizontal direction of movement $F_{H} \approx 28 \ N$ Case 3 Vertical suction gripper position, Example: $F_{H} = (\frac{m}{\mu}) x (g + a) x S$ vertical direction of movement (worst $F_{H} = (\frac{0.314 \text{ kg}}{0.1}) \text{ x (9.81 } \frac{\text{m}}{\text{s}^{2}} + 5 \frac{\text{m}}{\text{s}^{2}}) \text{ x 2}$ $F_{H} \approx 93 N$ **Result:** In accordance with the problem This value must be used for designing definition, the result of 93 N from the system. Case 3 must be taken into account, as the system also transports the workpiece in a vertical suction gripper position with vertical force. F_{H} = Theoretical holding force of the μ = Friction factor¹⁾ а = Acceleration of the system S Safety factor 0.1 for oily surfaces suction gripper [N] [m/s²] (minimum value is a safety = Mass [kg] factor of 1.5, for critical, non-0.2 ...0.3 for wet surfaces

- = Acceleration due to gravity g [9.81 m/s²]
- Note the emergency off acceleration.
- uniform or porous materials or rough surfaces the factor should be 2.0 or higher)
- 0.5 for wood, metal, glass, stone ... 0.6 for rough surfaces

1) The specified friction factors are average values and should be verified for the workpiece in question.

m

Step 3: Calculating the holding force and breakaway force

[N]

n

Determining the breakaway force F_A = Theoretical breakaway force

 F_H = Theoretical holding force of the

(2 suction grippers are planned in the problem

example)

suction gripper [N] (Result → 45) = Number of suction grippers

FESTO

Round suct	ion cup	F _A at −0.7 bar						1 сир	F _A at -0.7 I
Ordering data	Suction cup ∅	Standard	Extra deep	Bellows, 1.5 convol- utions	Bellows, 3.5 convol- utions	Orc dat	dering ta	Suction cup size	Oval
	[mm]							[mm]	
→ ess	2	0.1 N				→	ess	4x10	2 N
	4	0.4 N						4x20	3.4 N
	6	1.1 N						6x10	2.9 N
	8	2.3 N						6x20	5.9 N
	10	3.9 N		4.7 N	3.9 N		8x20	8 N	
	15	8.5 N	9.8 N					8x30	10.9
	20	16.3 N	17 N	12.9 N	8.2 N			10x30	15.2
	30	40.8 N	37.2 N	26.2 N	20.8 N			15x45	32 N
	40	69.6 N	67.6 N	52.3 N	42.4 N			20x60	62.8
	50	105.8 N	103.6 N	72.6 N	63.4 N			25x75	92.5
	60	166.1 N	162.5 N					30x90	134.4
	80	309.7 N	275 N	213.9 N					
	100	503.6 N	440.8 N						
	150	900 N							
	200	1,610 N							

Example:

 $F_{A} = \frac{93 \text{ N}}{2}$

 $F_A\approx 47~N$

Suction cup diameter too big for

workpiece

Reliable range for the problem example

Ψ

Breakaway force FA too low

In this example we opt for 2 suction grippers:

 $F_A = \frac{F_H}{n}$

• Round design

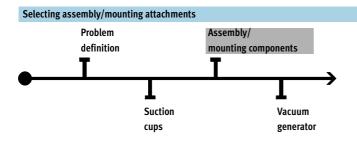
- Suction cup diameter 40 mm
- Breakaway force of 69.6 N



--Note

The load capacity of the vacuum suction gripper must be greater than the calculated value.

Introduction



Vacuum port

• top

at side

Check list

Workpiece Consideration of the workpiece

surface

- Angle compensator for very uneven surfaces
- Spring-mounted holders for sensitive workpieces as well as varying pick-up heights

Selecting the suction cup holder

The suction cup holder as well as the "angle compensator" and "vacuum filter" accessories are selected on the basis of the previously defined suction cup diameter. According to the problem example, the

workpieces must be picked up and set down with the aid of a spring. The vacuum lines should be attached at the side using push-in connectors. The suction grippers should be mounted with external threads.

Positioning of the vacuum tubing

- Spring-loaded holders:

 In the event of excess stroke and height tolerances, it is recommended that you use a holder with a height compensator – the same applies for sensitive workpieces that need to be placed gently and with the aid of a spring.
- Choice of vacuum ports 1:
 - top
- at side 3 connection types 1:

Type of connection

suction cup holder

fitting

Selecting the vacuum port for the

• Thread, push-in connector, barbed

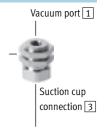
- Push-in connector QS
- Barbed fitting PK
 Thread G
- Different mounting threads for holder 2:
 - Female thread
 - Male thread

Round suction cup															
		From problem example													
									$\mathbf{\Lambda}$						
Suction cup \varnothing	2	4	6	8	10	15	20	30	40	50	60	80	100	150	200
[mm]															
Holder size	1		2		3 4		4	4		5		6			
Suction cup connection	3 mm		4 mm		M4x0.7	D.7 M6x1			M10x1		M10x1.	.5		M20x2	
3															
Ordering data	→ esh	→ esh													

Oval suction cup											
Suction cup size	4x10	4x20	6x10	6x20	8x20	8x30	10x30	15x45	20x60	25x75	30x90
[mm]											
Holder size	4	4 5									
Suction cup connection	M6x1	M6x1 M10x1.5									
3											
Ordering data	→ esh										

FESTO

Subject to change



Type of mounting

• Female/male thread

Mounting

threads for

holder 2

Mounting the suction cup holder on

the handling unit, e.g. robot arm

FESTO

er typ	De									
		From problem example								
		ili)	e]a	6209	-2000	110				
		HA	HB	HC	HCL	HD	HDL	HE	HF	
•	Height compensation	-	-					-		
	Vacuum port 1 Top		-			-	-			
•	At side	-		-	-			-	-	
•	Threaded connection G									
	Push-in connector QS							-	-	
	Barbed fitting PK							-	-	
		•	•	•	•				•	
	Mounting threads for hole	der 2								
	Female thread	-		-	-	-	-	-	-	
	Male thread		-							

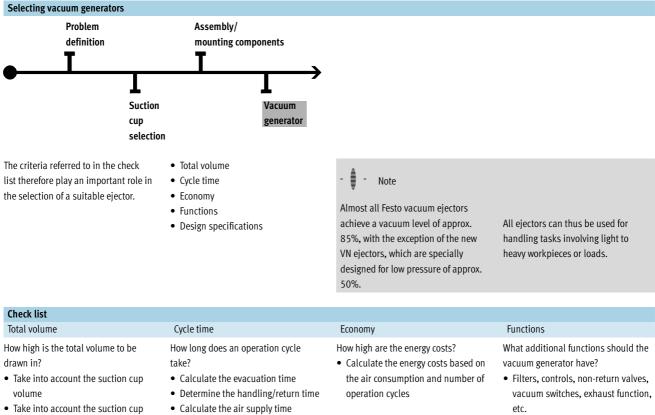
Result

Taking all requirements into account: Suction cup holder HD, size 4



FESTO

Introduction



- Take into account the suction cup holder volume
- Calculate the tube volume

Design specifications

What specifications exist?

• Dimensions, weight, mounting position, etc.

Step 1: Determining the total volume of the system (volume to be drawn in)

The suction cup, holder and tube volumes must be determined and added together to form the total volume.

Suction cup volume V_1	Suction cup holder volume V_2	Tube volume V ₃	Total volume V _T
The suction cup volumes are specified in the datasheet for the relevant vacuum suction grippers ESG, VAS, VASB. The suction cup volume may be specified in a table or chart, depending on the product family.	Because of the huge range of different holder types and connection options, tables listing all of the suction cups and their relevant volumes have been created in the datasheet for the ESG product family.	Once the suction cups, suction cup holders and connection options have been defined, the tube volume can be determined. Tubing PUN: Outside/inside Ø [mm]	$V_T = V_1 + V_2 + V_3$ $V_T = 3,132 + 678 + 12,566$ $V_T = 16,376 \text{ mm}^3 (16.38 \text{ cm}^3)$
In our sample application we opted	In our sample application we chose	3.0/2.1	
for 2 suction grippers:	the following suction cup holders:	4.0/2.6 6.0/4.0	
 Round design 	 Suction cup holder HD 	8.0/5.7	
 Suction cup diameter 40 mm Breakaway force of 69.6 N 	Size 4 with QS connector	10.0/7.0	
	$V_2 = 678 \text{ mm}^3$	The following formula must be used	
For these suction cups, the datasheet specifies a suction cup volume		when calculating the volume:	
of 1,566 mm ³ per suction cup.		$V_3 = \pi x \frac{D^2}{4} x L$	
V ₁ = 2 x 1,566 mm ³ = 3,132 mm ³		D = Tube inside ∅ [mm] L = Tube length [mm]	
		In the sample application a suction	

In the sample application a suctio cup holder with QS-6 couplings is used. A tube with an outside diameter of 6 mm is therefore required. In order to connect the vacuum generator to both suction cups, a tube length (L) of approx. 1 m (1,000 mm) is required.

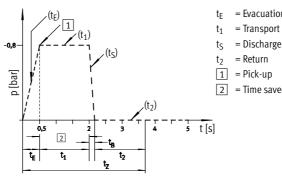
$$V_3 = \pi x \frac{4^2}{4} x 1000$$

 $V_3 = 12566 \text{ mm}^3$

Introduction

Step 2: Determining the cycle time

T_C = Evacuation time t_E + handling time t₁ + air supply time t_S + return time t₂



= Evacuation time

= Discharge

= Return

= Pick-up

= Time saved

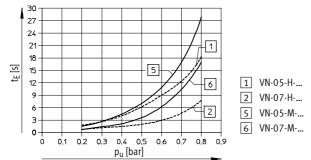
An operation cycle can be subdivided into individual time intervals, which must be either measured or calculated. The individual times added together produce the cycle time.

Evacuation time t_E

The evacuation time, i.e. the time taken for a volume to reach a certain vacuum level, is very useful for assessing the performance of a vacuum generator. The evacuation

time can be found in the datasheet of the relevant vacuum generator. This example depicts charts for some of the vacuum generators of the VN-... product family.

Evacuation time t_E for 1 litre volume at 6 bar operating pressure p_u



Calculation:

In Step 1 of the sample application we determined a total volume for the vacuum system of $V_T = 16.38 \text{ cm}^3$ (17 cm³). Using a basic rule of three, we can now calculate the evacuation time t_E for this system with any vacuum generator. According to the problem definition, $t_F < 0.5$ s, based on a vacuum level of 80%.

Example 1: VADMI-45 $t_{E} = V_{T} x t_{E1} / 1,000$ t_E = 17 cm³ x 25 s/1,000 cm³

t_E = 0.425 s (0.43 s)

Example 2: VADMI-70 $t_F = V_T \times t_{F1}/1,000$ t_F = 17 cm³ x 11 s/1,000 cm³

 $t_F = 0.187 \text{ s} (0.19 \text{ s})$

Example 3: VN-07-H $t_E = V_T x t_{E1}/1,000$ t_E = 17 cm³ x 8 s/1,000 cm³ t_E = 0.136 s (0.14 s)

Evacuation time (VT) tF

Evacuation time (V = 1,000 cm³) = t_{E1} Total volume (from example) VT

Handling time t₁

The time required to handle the workpiece after the end of the suction process (e.g. determined using a stopwatch = 1.5 s).

Air supply time ts

Time needed by the vacuum system to build up the pressure (vacuum) again and set down the workpiece. The air supply time can be found in the technical data for the relevant vacuum generator.

The specifications apply to 1 litre volume at 6 bar operating pressure at max. vacuum level.

Example 1: VADMI-45 $t_{S} = V_{T} x t_{S1} / 1,000$ ts= 17 cm³ x 1.9 s/1,000 cm³

 $t_{S} = 0.03 s$

Cycle time t_C

t_C = 3.46 s

Example 1: VADMI-45

 $t_{c} = t_{E} + t_{1} + t_{S} + t_{2}$

 $t_{C} = 0.43 + 1.5 + 0.03 + 1.5$

Using a basic rule of three, we can now calculate the air supply time t_S for this system.

Example 2: VADMI-70 $t_{S} = V_{T} x t_{S1} / 1,000$ ts= 17 cm³ x 0.59 s/1,000 cm³ ts= 0.01 s

Example 2: VADMI-70 $t_{c} = t_{E} + t_{1} + t_{S} + t_{2}$ $t_{C} = 0.19 + 1.5 + 0.01 + 1.5$ $t_{\rm C} = 3.2 \, {\rm s}$

Evacuation time (V_T) tς = Evacuation time ($V = 1.000 \text{ cm}^3$) ts1

Vт

= Total volume (from example)

Example 3: VN-07-H $t_{S} = V_{T} x t_{S1} / 1,000$ t_S= 17 cm³ x 1.1 s/1,000 cm³ ts= 0.02 s

Example 3: VN-07-H $t_{c} = t_{E} + t_{1} + t_{S} + t_{2}$ $t_{C} = 0.14 + 1.5 + 0.02 + 1.5$ t_C = 3.16 s

The time needed by the vacuum

Return time t₂

system to return to the initial position after the workpiece has been set down (e.g. determined using a stopwatch = 1.5 s).

Subject to change



Step 3: Checking economy of operation

Energy costs are determined on the basis of air consumption.

Determining the air consumption per operation cycle Q_C

	, ,		
These charts are also included in the datasheet for the relevant vacuum generator (e.g. VADM, VADMI). The VADMI vacuum generators have a built-in non-return valve which maintains the vacuum after the vacuum generator has been switched off (prerequisite: there must be no leakage in the system).	When combined with the vacuum switch it provides an air-saving function, i.e. no air is consumed during transport of the workpiece. The VN vacuum generators do not have this function. This means, therefore, that the vacuum generator remains in operation so that it can hold the workpiece during transport.	Air consumption Q as a function of oper	VADM-95 VADM-95 VADM-70 VADM-70 VADM-45
Qz = Air consumption per operation cycle t _E = Evacuation time for application Q = Air consumption per vacuum generator [l/min]	Example 1: VADMI-45 $Q_z = t_E x \frac{Q}{60}$ $Q_z = 0.43 \text{ s } x \frac{11 \text{ l}}{60 \text{ s}}$ $Q_z = 0.08 \text{ l}$	Example 2: VADMI-70 $Q_{z} = t_{E} \times \frac{Q}{60}$ $Q_{z} = 0.19 \text{ s } \times \frac{31 \text{ l}}{60 \text{ s}}$ $Q_{z} = 0.10 \text{ l}$	Example 3: VN-07-H $Q_{Z} = (t_{E} + t_{1}) \times \frac{Q}{60}$ $Q_{Z} = (0.13 \text{ s} + 1.5 \text{ s}) \times \frac{28 \text{ l}}{60 \text{ s}}$ $Q_{Z} = 0.76 \text{ l}$
Determining the number of operation c	ycles per hour Z _h		
Z _h = Operation cycles per hour t _Z = Time per operation cycle t _E = Evacuation time for application	Example 1: VADMI-45 $Z_{h} = \frac{3,600 \text{ s}}{t_{z}}$ $Z_{h} = \frac{3,600 \text{ s}}{3.46 \text{ s}}$ $Z_{h} = 1,040$	Example 2: VADMI-70 $Z_{h} = \frac{3,600 \text{ s}}{t_{z}}$ $Z_{h} = \frac{3,600 \text{ s}}{3.2 \text{ s}}$ $Z_{h} = 1,125$	Example 3: VN-07-H $Z_{h} = \frac{3,600 \text{ s}}{t_{z}}$ $Z_{h} = \frac{3,600 \text{ s}}{3.16 \text{ s}}$ $Z_{h} = 1,139$
Determining the air consumption per h	our Q _h		
$\begin{array}{llllllllllllllllllllllllllllllllllll$	Example 1: VADMI-45 $Q_h = Q_C \times C_h$ $Q_h = 0.08 \mid x 1,040$ $Q_h = 83.20 \mid (0.08 \text{ m}^3)$	Example 2: VADMI-70 $Q_h = Q_C \times C_h$ $Q_h = 0.10 \mid x \; 1,125$ $Q_h = 112.5 \mid (0.12 \text{ m}^3)$	Example 3: VN-07-H $Q_h = Q_C \times C_h$ $Q_h = 0.76 l \times 1,139$ $Q_h = 865.64 l (0.87 m3)$
Determining the energy costs per year k	KeA		
$ \begin{array}{lll} {K_{EA}} & = & Energy \mbox{ costs per year} \\ Q_h & = & Air \mbox{ consumption per hour} \end{array} $	Costs for compressed air ¹ : 1 m ³ at 7 bar: $\in 0.02/m^3$, at an electricity price of	$K_{EA} = Q_h x$ Compressed air costs	$s/m^3 x \frac{t_{operating}}{Day} x \frac{t_{operating}}{Year}$

€0.10/kWh

Vacuum generator	Air consumption per cycle Qz [l]	· · ·	Air consumption per hour Q _h [m ³]	Energy costs per year K _{EA} ²⁾ [€]
VADMI-45	0.08	1,040	0.08	5.76
VADMI-70	0.10	1,125	0.12	8.64
VN-07-H	0.76	1,139	0.87	62.63

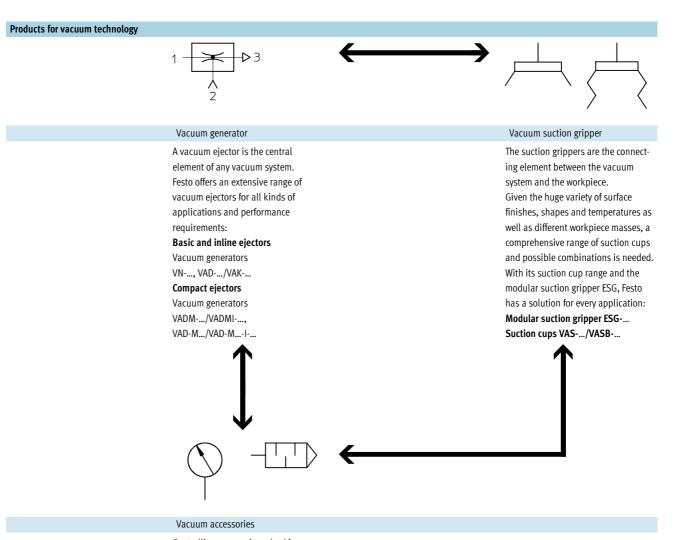
Material, depreciation and labour costs, etc. are reflected in the price
 Energy costs for shift operation 16 hours/day and 220 days/year

Introduction

Step 4: Taking additional functions/components and design specifications into account Selecting additional functions/components: and application of the system. All Selection of these components is guided by specific requirements in details regarding performance or terms of performance and functionalcomponents are provided in the ity, as well as by the place of operation datasheet on the relevant product. Solenoid valves Vacuum switch A vacuum system needs solenoid Operation cycles can be accelerated • Reliability through pressure valves for controlling vacuum and optimised by adding an extra Note monitoring • Adjustable switching point generation. These switch the vacuum valve as an ejector pulse generator. The nominal flow rate of the on and off. · Fast hysteresis adjustment solenoid valve must not be lower Vacuum generator Vacuum generator • Digital/analogue signal output than the suction capacity of the • VADM-..., VADMI-... • VADMI...- Display vacuum generator at atmospheric • VAD-M-..., VAD-M...-I-... • VADM...-I-... Ports pressure. (Both specifications can be found in the datasheet for the relevant product.) Filter Pressure gauge Silencers • Reliability: no contamination of the • Extension of the product life cycle • Manual pressure monitoring of the • Noise pollution kept to a minimum system and reduction of maintenance system intervals · Safety function Taking design specifications into account The following design specifications Size must be taken into account when Weight configuring a vacuum system: Resistance Calculation example summary Selection of suction cups Selecting assembly and mounting Selecting vacuum generators attachments The cycle time and economy of the Taking the mass and force The result takes all system We compared three vacuum ejectors were used as selection calculations plus all criteria into requirements into account: generators chosen at random from the criteria. account, we get the following result: Festo product range: Quantity 2 units Holder type HD Compact ejectors VADMI-45 Design round Size 4 VADMI-70 Suction $\sup \emptyset$ VN-07-H 40 mm Inline ejectors Breakaway force 69.4 N Material Polyurethane Result Cycle time Economy Compact ejector VADMI-45 All three vacuum generators lay within The vacuum generator VADMI-45 came The VADMI-45, on the other hand, has off best in terms of energy consumpa reasonable timeframe in the sample a smaller nozzle diameter and thus application and were below the tion and, consequently, energy costs. significantly lower air consumption. maximum time of 3.5 seconds The two compact ejectors VADMI-45 However, it cannot generate the specified in the problem definition. and VADMI-70 produced almost vacuum as quickly as the VADMI-70. identical results in relation to energy The number of cycles per unit of time and the quantities are almost costs. Although the larger VADMI-70 has a somewhat higher air consumpidentical for all three vacuum tion per unit of time, it can generate generators. the vacuum faster.

Introduction





Controlling, measuring, checking, filtering, etc. are important functions which, if not already included as standard in a vacuum system, can be added through an extensive range of accessories. Vacuum security valve ISV-... Vacuum gauges VAM-... Vacuum filters VAF-...

Vacuum switches VPEV-...

Other accessories: Height compensators, adapters Tubing QS push-in fittings